#### **Response to Anonymous Referee #1**

**Major comment**: Given that gas analyzers were used that simultaneously measure both CH4 and CO2, I really think that the authors should show the system's performance for CO2 as well. In L363, the authors write that have CO2 data but focus on CH4 for simplicity, but this choice makes life much less simple for all the researchers that want to measure both CH4 and CO2, and therefore need to do all the CO2 testing themselves. Showing the CO2 results would make this study much more useful and applicable for a much wider community, and certainly render more citations to this paper. At the very minimum, include the CO2 performance tests in the supplementary information, but I'd rather see that the CO2 data is fully integrated in the paper, including the title.

**Response**: We totally agree with the reviewer that CO2 should be included in the manuscript. We integrated CO2 results in the manuscript and mention CO2 in the title as well. Please see the manuscript.

#### Minor comments:

Title: Include "carbon dioxide".

Response: We included CO2 in the revised manuscript.

L13. Freshwater lakes and reservoirs are aquatic systems, so that's a repetitive formulation. Simplify.

**Response**: We deleted "in freshwater lakes and reservoirs" in Line 13. Please see line 14-15 in the revision.

L48-49. This sentence omits that dissolved CH4 concentration is very strongly a function of methanogenesis, this should be added.

**Response**: We added "In addition to formation processes that lead to CH4 accumulation" in the revised manuscript. Please see line 61-62 in the revision.

L69. Not only phytoplankton, but also other microbial life forms. I suggest to reword to "biological".

**Response**: We agree that many microorganisms might be involved and thus the word "biological" is more appropriate. We made this change in the revised manuscript (Line 91 in the marked revision).

Figure 1. The heart of the equilibrator is the gas-water mixing unit, and the gas-water separation unit. These should be illustrated much more clearly, as a technical drawing, such that people can build them themselves. The pictures in the SI don't really help very much.

**Response**: We have replaced Figure S1 with a technical drawing in which the gas-water mixing unit and the gas-water separation unit were both described in detail.

#### L150-154. This text could go to the figure caption.

**Response**: This text has been removed from the main text and now is part of the figure caption. Please see line 172-176 in the revision.

#### L155. Use full word "Laboratory"

**Response**: We changed "Lab" to "Laboratory". Please see line 177.

L178. The 13 m tubing length is not mentioned in this list, but it's shown in the figures. **Response**: Thanks for pointing this out. We added 13 m to the text. Please see line 204.

#### L193. Mention which these various methods were.

**Response**: We described explicitly what the methods are in the text. Please see line 218-219.

# L204. From what I read, the depth from which peristaltic pumps can pump up water is physically limited to about 14 m. So how come you could pump water from 30 m depth?

**Response**: Pump head that the pump needs to overcome is related to vertical distance of the pump to water surface only and unrelated to the vertical position of water intake below the water surface. Thus, often there is only < 0.5 m pump head when the FaRAGE is placed in a small boat.

L210. Was the effect of boat speed on equilibration tested? Depending on the type and placement of water intake, bubbles might start to form when driving too fast.

**Response**: We did not try higher boat speed than 10 km h-1. The driving speed should be chosen according to the spatial resolution that the users would like to have. In our case, 17 m spatial resolution (spatially averaged) was achieved at 5 km h-1 driving speed corresponding to 12 s response time (see line 377-378). Bubbles were not observed at 10 km h-1 speed when the water intake is mounted on the side wall of the boat, 0.5 m below the water surface. Driving too fast is not recommended as it may harm the CTD probe as well.

#### L229. Please give this correction equation.

**Response**: The correction equations for CH4 and CO2 are shown in Fig. 2a and b, respectively.

# L255. No details on statistical methods or tests are given, yet it says "significantly" here. Which test were performed, and what test statistics did they return?

**Response**: Thanks. Indeed, statistical tests were not performed. We changed this word to "substantially" and gave mean ± standard deviation. Please see line 289-290.

L260. Please rephrase, "while extended response times" is unclear. Fig.2, panel d. Change the right y-axis colour to red (such as in panel c). Also, why is the red point for 13 m tubing length not connected to the other red points, and how come that its response time is so much longer for high-to-low than for low-to-high, and also so much longer than for the 8 m tubing? **Response**: Thanks. This is an incomplete sentence. We rephrased the sentence to "A 91.8% equilibration ratio can be achieved by extending the tube length to 13 m while extended response times are expected."

We have changed the right-handed y-axis color to red in panel d. Please see the new Fig. 3c-d. The red point for the 13 m tube length severely deviated from the well-fitted power function. The sharp increase in response time of high-to-low is a result of increased resistance of the gaswater mixture flow. The instability (abnormal sharp increase in response time) started from 13 m tube length and became unacceptable when the tube length is 18 m. Please see our explanations in line 294-302. L373. I would be more careful with this statement. You can state that the equilibrator was not negatively affected by high phytoplankton density, but you haven't tested suspended sediment, so it's not sure it would work in e.g. in a turbid river. You can't exclude that for sustained operation in a turbid system, a filter in the water intake might be required.

**Response**: Thanks. Indeed, so far the device has never been tested particularly in turbid rivers with suspended sediment particles. We confined this statement to lakes without high sediment loads and also pointed out explicitly that a filtration unit for the water intake might be needed in turbid rivers. Please see line 427-433.

#### L383. Unclear what this sentence means, please rephrase.

**Response**: Thanks. They are indeed misleading and unnecessary, therefore, we have removed them from the manuscript.

#### L408. "potentially be" instead of "be potential".

Response: We corrected this in the text. Please see line 466.

#### Supporting information:

L32. Coupling instead of couple. **Response**: We corrected this in the text (line 33).

Fig.S1. The pictures of the syringes don't show much, and don't help those who want to build their own. Use better pictures and include a technical drawing.

**Response**: We improved these by replacing them with technical drawings.

L120. This is not a complete sentence. **Response**: Thanks. We rephrased this sentence. Please see line 127-128.

Fig.S3. Please also show the corresponding depth profiles of CH4 and CO2 at this sampling occasion, such that the reader can judge in how far phytoplankton density might have affected measurements.

**Response**: We added depth profiles of CH4 and CO2 to Fig. S3.

#### **Response to Anonymous Referee #2**

## I have two remarks to be considered and few suggestions

1) I was very interested in the CH4 profiles and - while impressed by the high vertical resolution they achieve – I understood the authors tested their system in different lakes, covering some "typical" methane concentration range. Indeed they show two profiles: one from mesooligotrophic Lake Stechlin and one from eutrophic Lake Arend - I supposed they choose trophic state as a proxy for GHG content (Beaulieu et al., 2019). Thus I was confused seeing that Lake Arend, that they present as eutrophic, shows especially low methane, even lower than what they show for the meso-oligotrophic (Lake Stechlin). So what is the criterion behind this choice? Why picking an eutrophic lake that has even less methane than the meso-oligotrophic? Why not a typical eutrophic lake with methane building up below the oxycline during summer stratification? (They show a large literature on this issue in the Intro). For calibration the authors limited the upper range of methane to <2 micromoles L-1. While for high concentrations (microM to mM range) the authors suggest dilutions (line 357) but they don't deal with the problem in this paper. I think the range they show is fair enough, but they should clarify this "lower range test", directly relatable to surface waters but not to littoral methane rich or eutrophic lake bottom waters, AND change the sentence in the abstract "The FaRAGE is capable of continuously measuring dissolved CH4 concentrations in the nM-to-mM range" as it may be capable of that, but is not shown here.

## Response:

Thanks for the reviewer's very detailed comments. We have such CH4 profiles with a typical anoxic hypolimnion in summer where CH4 was enriched to sub milli-molar high concentration. We have added these data into the revised manuscript. Please see Fig. 4c-d.

We further added additional laboratory tests for high CH4 concentration (e.g., 33  $\mu$ M). The measured concentration is about 245 ppm with the FaRAGE. For the Gas Scouter 4301 we use, linearity can only be guaranteed up to 500 ppm. Adjustment of water-gas mixing ratio is needed for CH4 concentrations in the mM range. Therefore, we agree with the reviewer's suggestion. We rephrased the measurement range-related statement accordingly.

2) One big step forward the authors claim is the "extraordinary fast response relative to all existing gas equilibration devices" (line 274). However, when their system is used with PICARRO G2132-1 + a desiccant to measure stable isotopes of gas species, it does not get that much faster than Hartmann 2018 "High Spatio-Temporal Dynamics of Methane Production and Emission in Oxic Surface Water" (line 107 of supplementary material). If I understand correctly then, what showed in table S4 is not entirely correct since their system response time when using PICARRO G2132-1 is obtained without any dryer. As far as I know, for using a PICARRO G2132-1 with a moisty flow a dryer is absolutely necessary. How humid is the water entering the analyzer? In case the authors think that a dryer is needed, they should change the table S4 and the statement in line 274 "The comparison between up-to-date previous studies and this study (Table S4) demonstrated the extraordinary fast response relative to all existing gas equilibration devices. A 53 s response time was achieved when the FaRAGE was adapted to the Picarro G2132-i, which is significantly faster than others (171-6744 s)."

## Response:

Thanks for suggesting this. We did not have appropriate dryers for testing when the tests were performed. Therefore a dryer made from silicone beads was tested and a 150 s extension in response time was observed. But we are aware that this has been well tested in Webb et al (2016), in which they tested both Drierite and magnesium perchlorate (Mg(ClO4)2) as dryers. We reproduced their results below. They show both types of dryer have no effect on CH4 and CO2, except for a 1.5 min time delay on CO2 was caused by using Drierite.

Yes, the water vapor content of the gas sample flow is above 1% and should be dried before entering the PICARRO G2132-i. We are currently using the drying materials as suggested by Webb et al (2016) and they work quite well.

So the numbers in table S4 and the statement in line 274 are all valid. We understand it is not well clarified. We clarified this in the revised version of the manuscript. Please see the revision in line 113-117 in the supporting information.

## Reference

Webb, J. R., Maher, D. T., and Santos, I. R.: Automated, in situ measurements of dissolved CO<sub>2</sub>, CH<sub>4</sub>, and  $\delta_{13}$  C values using cavity enhanced laser absorption spectrometry: Comparing response times of air-water equilibrators, Limnol. Oceanogr.: Methods, 14, 323-337, https://doi.org/10.1002/lom3.10092, 2016.



**Fig. 2.** Step experiments carried out to determine the effect of two desiccants, Drierite (**A**) and magnesium perchlorate (Mg(ClO<sub>4</sub>)<sub>2</sub>) (**B**), on the response times of CO<sub>2</sub> and CH<sub>4</sub> through a showerhead equilibrator. A time delay of 1.5 min was observed for CO<sub>2</sub> concentrations when Drierite was used as a desiccant. Mg(ClO<sub>4</sub>)<sub>2</sub> had no effect on concentration response times and CH<sub>4</sub> remained unaffected by both desiccants.

# Suggestions

When describing the set up the authors often refer to a "bubble unit", which I suppose in the scheme (Fig.1) is called "gas-water mixing unit". Consider harmonize.

#### Response:

Thanks for pointing this out. We checked this carefully and now the terms are used consistently throughout the manuscript.

Line 363- I think it would be better to rephrase the reason why CO2 is not shown. "for simplicity" for them or for the reader? Maybe they can mention which non-simple problems we meet when applying the system to CO2.

#### Response:

We have added CO2 as well and incorporated it throughout the full manuscript.

As to line 366 it is possible for the authors to use their system at sea enhancing the liquid to HS ratio to achieve low concentrations.

# Response:

Thanks for suggesting this. We replaced one calibration point in Fig. 2, in which 5.5 nM dissolved CH4 concentration can be well characterized (with the 500 mL min-1 to 1000 mL min-1 water-gas mixing ratio). Indeed, lower concentrations in the ocean system can be also well measured by increasing water-gas mixing ratio.

I would recommend to make sure that the scientific community that works on GHG airwater exchange in oceans gets interested too (add to abstract and line 97?). For different reasons from the ones highlighted here for inland waters (to name one the massive lack of ground data to calibrate satellite infers) this system could be applied to voluntary observing ship programs to map CO2 and CH4 surface concentrations. In case the authors find a major obstacle to this it would be good to mention – making a suggestion for adapting their system for oceanographic applications.

## Response:

Thanks for suggesting these. We agree that the FaRAGE can be a good method for studying GHGs from oceans. We added a sentence in abstract (line 35-36) and also in text (line 117-118).

Line 382- they mention how temperature should be corrected for the change along the hose- can give an example on how off can it get and does that mean to always measure temperature in situ at depth along with the profile?

# Response:

We included an example in SI (Fig. S4) to show how much the water temperature (water flow inside the gas-water separation unit) can differ from the in situ water temperature. It's more important to monitor temperature of water flow inside the gas-water separation unit of the device. We recommend to installing a temperature logger in the device if someone would like to rebuild the device, but can only afford one thermometer.

# Line 400 replace "filthy"

# Response:

Thanks. We rephrased this sentence (see line 458).

Line 410- wouldn't a scrubber serve for that? Would that slow down the system RT?

#### Response:

Thanks. Yes, a copper scrubber can help to remove H2S from the gas samples (Malowany et al. 2015). According to Malowany et al. (2015), no time delay was observed when a copper scrubber was used. We also reproduced the figure they included in the publication. We added this reference to the revised manuscript (line 469-471).

#### Reference

Malowany, K., Stix, J., Van Pelt, A., and Lucic, G.: H2S interference on CO2 isotopic measurements using a Picarro G1101-i cavity ring-down spectrometer, Atmos. Meas. Tech., 8, 4075–4082, https://doi.org/10.5194/amt-8-4075-2015, 2015.



**Figure 3.** Change in the <sup>12</sup>CO<sub>2</sub> and <sup>13</sup>CO<sub>2</sub> concentrations with addition of H<sub>2</sub>S to the standard gas. (a) Plot showing the percentage change in CO<sub>2</sub> concentration between gas with H<sub>2</sub>S and gas scrubbed of H<sub>2</sub>S. There is a visible increase in the <sup>12</sup>CO<sub>2</sub> concentration and a decrease in the <sup>13</sup>CO<sub>2</sub> concentration with addition of H<sub>2</sub>S. The percentage decrease for <sup>13</sup>CO<sub>2</sub> is significantly greater than the percentage increase for <sup>12</sup>CO<sub>2</sub>. (b) Plot showing the 1000 ppm standard CO<sub>2</sub> gas with the addition of 3 mL of 100 ppm H<sub>2</sub>S and the subsequent response after the H<sub>2</sub>S was removed with the copper scrub. There is a small, yet visible, increase in the <sup>13</sup>CO<sub>2</sub> concentration and decrease in the <sup>12</sup>CO<sub>2</sub> concentration when H<sub>2</sub>S is removed.

## References

Beaulieu, J.J., DelSontro, T. & Downing, J.A. Eutrophication will increase methane emissions from lakes and impoundments during the 21st century. Nat Commun 10, 1375 (2019). https://doi.org/10.1038/s41467-019-09100-5

1	A Fast-response automated gas equilibrator (FaRAGE) for continuous in situ
2	measurement of methane-CH4 and CO2 dissolved in water
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12	Abstract
13	Biogenic greenhouse gas methane (CH4) emissions, e.g. of methane (CH4) and carbon
14	dioxide (CO <sub>2</sub> ) from inland waters contribute substantially to global warming. In aquatic systems,
15	dissolved CH4- in freshwater lakes and reservoirs is-greenhouse gases are highly heterogeneous
16	both in space and time. To better understand the biological and physical processes that affect
17	sources and sinks of <u>both CH4 and CO2</u> in lakes and reservoirs, <u>itstheir</u> dissolved CH4
18	<u>concentrations</u> needs to be measured with a highest <u>spatial and</u> temporal resolution. To achieve
19	this goal, we developed the Fast-Response Automated Gas Equilibrator (FaRAGE) for real-
20	time in situ measurement of dissolved CH4 and CO2 concentrations at the water surface and in
21	the water column. FaRAGE can achieve an exceptionally short response time ( $t_{95\%} = 12$ s when

- including the response time of the gas analyzer) while retaining an equilibration ratio of  $\frac{6362.6}{63}$ %
- and a measurement accuracy of 0.5% for CH<sub>4</sub>. A similar performance was observed for

dissolved CO<sub>2</sub> ( $t_{95\%} = 10$  s, equilibration ratio 67.1%). An equilibration ratio, as high as 91.8%, 24 can be reached at the cost of a slightly increased response time (16 s). The FaRAGE is capable 25 of continuously measuring dissolved CO2 and CH4 concentrations in the nM-to-sub mM (10-9 -26  $10^{-3}$  mol L<sup>-1</sup>) range with a detection limit of sub-nM ( $10^{-10}$  mol L<sup>-1</sup>), when couplinged with a 27 cavity ring-down greenhouse gas analyzer (Picarro GasScouter). It enables the possibility of 28 mapping dissolved CH<sub>4</sub> concentration in a "quasi" three-dimensional manner in lakes. 29 Additional tests demonstrated a sSimilarly good performance of FaRAGEthe equilibrator could 30 be demonstrated for measuring dissolved CO<sub>2</sub>. FaRAGE enables allows for the possibility of 31 mapping dissolved concentration in a "quasi" three-dimensional manner in lakes and The 32 33 FaRAGE provides an inexpensive alternative forto other commercial gas equilibrators. It is simple to operate and suitable for continuous monitoring with a strong tolerance to suspended 34 particles. While the FaRAGE is developed for inland waters, it can be also applied to ocean 35 36 waters by slightly tuning the gas-water mixing ratio. The FaRAGE is e easy adaptability easily adapted to suit to other gas analyzers such as Ultra-portable Los Gatos and stable isotopic gas 37 analyzer (Picarro G2132-i) also provides the potential for many further expanding the range of 38 potential applications, including nitrous oxide and isotopic composition of the gases.e.g. 39 measuring dissolved <sup>13</sup> & C-CH4 and <sup>13</sup> & C-CO2 and CO2. 40

41

## 42 **1 Introduction**

Despite the well-established perception of inland waters as a substantial source of 43 atmospheric methane (CH<sub>4</sub>) and carbon dioxide (CO<sub>2</sub>) (Bastviken et al., 2011; Cole et al., 2007; 44 Tranvik et al., 2009), the magnitude of these greenhouse gases remains large uncertainties 45 46 uncertain owing to the fact that poorly constrained some key processes affecting CH<sub>4</sub> (e.g. bubbling) and CO<sub>2</sub> budget are still poorly constrained sources and sinks (Saunois et al., 2019). 47 Most freshwater lakes and reservoirs are often oversaturated with CH<sub>4</sub> and CO<sub>2</sub> (relative to 48 49 atmosphere) and their distribution are characterized by high spatio-temporal heterogeneity (Hofmann, 2013). Point-based and short-term measurements can result in biases in estimating 50 diffusive CH<sub>4</sub> flux (Paranaíba et al., 2018). Thus, resolving the spatio-temporal dynamics of 51 both dissolved CH<sub>4</sub> and CO<sub>2</sub> concentration in lake water is a prerequisite for a better budgeting 52 understanding of sources and sinksproduction and loss processes of these gases in freshwater 53 54 lakes.

The distribution of CH<sub>4</sub> and CO<sub>2</sub> in lakes is often characterized by pronounced vertical 55 and horizontal concentration gradients, which can occur either below or above often coincides 56 with the position of the thermocline. In many deep stratified lakes, a sharp vertical gradient of 57 58 <u>CH4, for instance</u>, below the thermocline can develop in the anoxic hypolimnion (mM range) (Encinas Fernández et al., 2014; Liu et al., 1996). In contrast, in some stratified lakes with a 59 fully oxygenated hypolimnion CH<sub>4</sub> can accumulate above the thermocline (~µM range) 60 (Grossart et al., 2011; Donis et al., 2017; Günthel et al., 2019). In addition to formation 61 processes that lead to CH<sub>4</sub> accumulation, the concentration of dissolved CH<sub>4</sub> is also regulated 62 by losses due to oxidation and emission to the atmosphere (Bastviken et al., 2004; Juutinen et 63 al., 2009). Both rates can be Particularly the eEmission rates, in particular, are highly variable, 64 65 particularly for the flux term as which is strongly affectedit depends dependent by on turbulence generated induced by wind and or convective mixing (Read et al., 2012; Vachon and Prairie, 66

67 2013). In addition to the uneven vVertical CH4-distributions of CH4 and CO2, can be further
68 confounded the contribution of littoral sediments which can result in distinct horizontal
69 gradients of CO2 and CH4 - apparent horizontal gradients have been observed in lakes where
70 littoral sediments are identified as a CH4 source (Murase et al., 2003). This Accounting for
71 horizontal CH4-gradients can also therefore critical as lateral transport may account for
72 contribute to the a proportion of the epilimnetic CH4 peak observed in pelagic waters via lateral
73 transport (Hofmann et al., 2010; Fernández et al., 2016; Murase et al., 2005; Peeters et al., 2019).

74 These spatial Spatial pattern distributions of CH4 and CO2 in aquatic systems, however, are subject to temporal variation in response to vary over time, particularly as factors which 75 control their production, consumption and loss to the atmosphere fluctuate. variable drivers as 76 well as water motion. Nevertheless, dissolved CH4 in lake water is not only featured with 77 variable spatial patterns, it also changes at different time scales as most processes that contribute 78 to the spatial heterogeneity are not always synchronized. The rise and fall of ILake CH4 79 concentration Concentrations of CH<sub>4</sub> and CO<sub>2</sub> in lakes demonstrate often show strong profound 80 seasonality, that are is driven primarily by thermal stratification (Encinas Fernández et al., 2014) 81 and phytoplankton dynamics (Günthel et al., 2019). While the build-up of hypolimnetic CH<sub>4</sub> 82 83 storage is a slow process that is closely related to the development of lake hypoxia, the epilimnetic CH4 and CO2 maximum can be highly variable even at a daily basis as it is they are 84 strongly affected by phytoplankton dynamics (Günthel et al., 2019; Hartmann et al., 2020; Bižić 85 86 et al., 2020). In addition, storms can act as another driver for short-term CH4-dissolved gas dynamics in the lake because it-they often leads-contribute to higher evasion rates caused by 87 88 strong vertical turbulent mixing (Zimmermann et al., 2019) and enhanced horizontal transport (Fernández et al., 2016). While the seasonal patterns of dissolved CH<sub>4</sub> and CO<sub>2</sub> concentration 89 in lake water seem recurrent and can be simulated (Stepanenko et al., 2016), the unpredictable 90

91 effects of short-term <u>phytoplankton\_biological</u> dynamics and storm events can present a
92 challenge in modeling <u>lake CH4-the</u> dynamics of greenhouse gases in lakes.

While there is an urgent need for resolving the spatio-temporal variabilities variability 93 94 of CH<sub>4</sub> in large water bodies (e.g. deep, stratified lakes), we recognize limitations in the 95 available methodology. Like most gases in dissolved phase, CH<sub>4</sub> and CO<sub>2</sub> cannot be measured directly in water. Instead, a carrier gas (synthetic air or at air concentration) is added to achieve 96 (full/partial) gas-water equilibration. The headspace gas sample is then measured with a gas 97 98 spectrometer and the concentration of targeted gas can be calculated according to Henry's law (Magen et al., 2014). To save sampling effort, continuous gas equilibration devices have been 99 100 developed, which generally can be classified to in four categories: 1) Membrane type (Schlüter 101 and Gentz, 2008; Boulart et al., 2010; Gonzalez-Valencia et al., 2014; Hartmann et al., 2018) -102 gases are extracted from water by-using a gas-permeable membrane; 2) Marble type (Frankignoulle et al., 2001; Santos et al., 2012) - gas exchange is enhanced by pumping water 103 104 through marbles that increases the gas-water contact area; 3) Bubble type (Schneider et al., 1992; Körtzinger et al., 1996; Gülzow et al., 2011) - dissolved gases are stripped out by 105 106 bubbling the water sample; 4) Showerhead type (Weiss-type) (Johnson, 1999; Rhee et al., 2009; Li et al., 2015) - water is pumped from top and then mixed with a circulated headspace carrier 107 gas. A full evaluation on the performance of these devices was provided in a recent review 108 (Webb et al., 2016), where, the most important paprameter, response time, was found to vary 109 between 2-34 min for dissolved CH<sub>4</sub>. While it is already encouraging, improvements are 110 111 expected to further shorten the response time.

Driven by the need to resolve temporal and spatial variabilities variability of dissolved CH4 and CO<sub>2</sub> in inland waters lakes or /reservoirs with sufficient precision, we developed a novel, low-cost equilibrator to achieve fast gas-water equilibration. The **Fast-Response Automated Gas Equilibrator (FaRAGE)** can be coupled with a portable gas analyzer, which makes it perfect for field use. Here, the performance of the FaRAGE is evaluated by investigating its response time, detection limit and equilibration ratio. <u>Although FaRAGE is</u> <u>developed for inland waters, it can be also adapted for oceanographic applications</u>. Applications are provided exemplarily to demonstrate the potential of the FaRAGE for improving our understanding on the spatial distribution and temporal dynamics of dissolved CH<sub>4</sub> and CO<sub>2</sub> in inland waters.

### 122 2 Materials and Methods

## 123 **2.1 Device description**

The design of the FaRAGE is modified from two types of equilibrators: Bubble-type (Schneider et al., 1992) and Weiss-type (Johnson, 1999). In contrast to the traditional bubbletype and Weiss-type equilibrators that create a large-volume headspace and circulates air back to the headspace, the FaRAGE is a flow-through system that adds gas flow into a constant water flow to produce a minimal headspace for continuous concentration measurement of <u>CO<sub>2</sub> and</u> CH<sub>4</sub> dissolved in water.

130 The operation principle of the FaRAGE is depicted in Fig. 1 and photos technical drawings of the main parts of the prototype are provided in Fig. S1. A list of information on 131 suppliers and cost of each part can be found in Table S1. A mass flow controller (SIERRA 132 C50L, Netherlands) is used to generate a constant carrier gas (normal air/synthetic air) flow (1 133 134 L min<sup>-1</sup>) from a compressed air tank coupled with a pressure regulator. Water samples are taken continuously using a peristaltic pump (500 mL min<sup>-1</sup>), and the flow is monitored using a flow 135 meter (Brooks Instrument, Germany). The two flows mix in a gas-water mixing unit that is 136 137 composed of a gas bubble generating unit and then travel through a coiled hose for further gaswater turbulent mixing. In the gas-water mixing unit bubble unit (modified from a 10 mL plastic 138 syringe), a jet flow is created by adapting narrowed tubing (2 mm inner diameter) to the water 139

pumping hose (3.2 mm inner diameter). Degassing occurs when the jet flow enters the chamber 140 141 with a sudden enlarged diameter (14 mm). Degassing is further enhanced by micro-bubbles that are generated by a bubble diffusor attached to the carrier gas hose (inside the bubble unitplastic 142 143 syringe). The gas-water mixture flows through the 2-m long Tygon tube (3.2 mm inner diameter) where additional equilibration occurs. The flow is finally introduced to a gas-water separation 144 unit (a 30 mL plastic syringe) where the headspace gas is separated from the water. In this 145 146 chamber, water falls down freely to the bottom while the headspace gas is taken directly to a greenhouse gas analyzer (1 L min<sup>-1</sup> gas pumping rate; GasScouter G4301, Picarro, USA). A 2-147 m long Tygon tube (3.2 mm inner diameter) is attached to the top of the chamber for venting 148 149 excess gas flow while stabilizing gas pressure in the headspace. The bottom water is discharged back to the lake using another peristaltic pump (500 mL min<sup>-1</sup>). To protect the gas analyzer 150 151 from damaging high water vapor content, a Teflon membrane filter (pore size 0.2 µm) is placed before the gas intake (resulting in a  $\sim 210$  mL min<sup>-1</sup> reduction in flow rate of gas sample, which 152 153 is vented from the bypass at the top of the gas separation unit). A desiccant (a 20 mL plastic syringe filled with dried silicone beads) is used to reduce moisture concentration to < 0.1%154 when attaching to a Picarro G2132-i isotope analyzer (Picarro, USA), in which < 1% moisture 155 level is required for  ${}^{13}\delta$ C-CH<sub>4</sub> measurement. The temperature of the water sample at the point 156 157 of equilibration with the headspace gas is monitored using a fast thermometer (precision 0.001 °C, 1 Hz, TR-1050, RBR, Canada) attached to the end of the water discharging hose. 158

As concerns might arise from the availability of gas analyzer coupled to the FaRAGE, iIn addition to Gas Scouter from Picarro, two additional widely used models of greenhouse gas analyzers were tested. They are the Ultraportable Los Gatos (Los Gatos Research, USA) and stable isotopic CH<sub>4</sub> analyzer (G2132-i, Picarro, USA). The main technical details of all three tested gas analyzers are listed in Table S2.





Fig. 1 Schematic design of the FaRAGE. The components include: Air tank containing 165 166 compressed carrier gas (air or synthetic air) with a pressure regulator, a mass flow controller (MFC) for generating constant carrier gas flow, two peristaltic pumps for taking and 167 discharging water, respectively, a flow meter for monitoring water sample flow, a gas-water 168 mixing unit, a gas-water separation unit, a gas analyzer, and a thermometer for measuring water 169 temperature at phase equilibration. A Teflon membrane filter is placed after the MFC and 170 another is added before the gas analyzer to protect from being flooded. A desiccant is used to 171 172 dry the gas flowing to the gas analyzer (if Picarro isotopic analyzer is used). The red color marks the flow of carrier gas, dark blue line indicates the water sample, purple line shows the 173 flow of gas-water mixture, the light brown line shows the flow of gas sample (after partial 174 175 equilibration) and the light blue line depicts the water discharged back to lake. The thickness of the lines scales with the gas/water flow rates. The arrows show the flow directions. 176

### 177 **2.2 Lab<u>oratory</u> validation**

The FaRAGE prototype was first tested intensively in the laboratory to determine both 178 the equilibration ratio and response time. The tests were performed for both CH<sub>4</sub> and CO<sub>2</sub> 179 aswith a GasScouter G4301 (Picarro, USA), which measures both gases simultaneously. For 180 simplicity, only the results for one gas (CH4) areis explained in the following text. The 181 equilibration ratio is defined as the percentage concentration of the gaseous CH4gas 182 concentrations at the outlet of the gas equilibrator in comparison to the equilibrium 183 184 concentration (full gas-water equilibration). The equilibration ratio was established by-across measuring a range of CH4-stock solutions (nano-to-milli molar dissolved gas concentrations). 185 These standard solutions were prepared by adding different amounts of either CH<sub>4</sub> or CO<sub>2</sub> into 186 a 200 mL headspace of a 2 L Schott bottle filled with Milli-Q water. The exact-dissolved CH4 187 concentrations in these solutions were tested with the traditional manual headspace method: a 188 400 mL headspace was created in a 500 mL plastic syringe with nitrogen gas. The CH4-gas 189 190 concentration of the headspace gas was then measured using GasScouter G4301 (Picarro, USA). At the same time, CH4-dissolved CH4 and CO2 concentrations of these standard solutions were 191 192 measured with the FaRAGE for at least 2 min and an average was calculated from more than 193 60 individual data points. We directly compared dissolved CH4-gas concentrations measured using the two different methods, i.e., our equilibrator and manual headspace method. 194

The response time of the device was investigated by switching the water sample inlet between two water samples with different CH<sub>4</sub>-concentrations <u>of either CH<sub>4</sub> or CO<sub>2</sub></u>. Triplicated measurements were performed. An exponential fit was applied to the concentration change curve and the response time was determined as time needed to reach 95% of the final concentration.

The effect of water-to-gas mixing ratio on equilibration ratio and response time of the device was investigated. By fixing the carrier gas flow rate to 1 L min<sup>-1</sup>, the water-to-gas mixing ratio was varied from 0.04, 0.08, 0.12, 0.15, 0.24, 0.29, 0.36, 0.43 and 0.5 by adjusting the water
sample flow rate. The effect of tube length on performance of the device was also examined by
adapting 1, 2, 4.4, and 8.4 and 13 m Tygon tube onto the gas-water mixing unit. For all these
tests, triplicated measurements of the equilibration ratio and response time were performed
corresponding to different mixing ratios and the mean values were used for analysis.

Tests were performed to investigate the performance of the device when adapting to two other types of gas analyzers. As the equilibration ratio is unaffected by the model of gas analyzers, only response time was determined. This was done by fixing carrier gas and water sample flow rates to 1 and 0.5 L min<sup>-1</sup>, respectively. The surplus gas was vented to the air as Ultraportable Los Gatos and Picarro G2132-i have a gas intake flow rate of only 500 and 25 mL min<sup>-1</sup>, respectively. The effect of desiccant on response time of Picarro G2132-i was checked by measuring gas samples with and without a desiccant installed.

#### 214 **2.3 Field tests**

215 Two-Four lakes in Germany were chosen for field tests. Lake Stechlin is a deep mesooligotrophic lake with a maximum depth of 68 m and Lake Arend is a eutrophic lake with a 216 maximum depth of 48 m. Pronounced CH<sub>4</sub> peaks in the epilimnion of Lake Stechlin have been 217 previously reported that were measured with various two different methods (manual headspace 218 method in Grossart et al. (2011) and Tang et al. (2014); membrane-based gas equilibrator in 219 Hartmann et al. (2018)). This makes it ideal for our testing purpose. While CH<sub>4</sub> profiles at Lake 220 Arend have never been reported, the metalimnetic oxygen minimum in the lake observed during 221 222 summer (Kreling et al., 2017) renders it interesting for CH<sub>4</sub> profiling throughout the entire water column. Another two-Additionally, we selected both eutrophic lakes with an anoxic 223 224 hypolimnion lakes (Lake Großer Pälitz and Lake Zotzen), where CH4 and CO2 can accumulate 225 are both eutrophic with an anoxic hypolimnion during the period of thermal stratification. 226 <u>Measurements were conducted in these two lakes to test the capability of FaRAGE to measure</u>
 227 anoxic hypolimnetic water with high dissolved CH<sub>4</sub> and CO<sub>2</sub> accumulated concentrations.

....

Due to the high potential of the FaRAGE for real-time in situ measurement of dissolved 228 229 CH<sub>4</sub> and CO<sub>2</sub> concentrations, we explored potential field applications. These field tests included 230 depth profiling of dissolved CH4 concentrations in Lake Arend and Lake Stechlin the four lakes and investigations of the horizontal distribution of surface dissolved CH<sub>4</sub> and CO<sub>2</sub> 231 concentrations across the entire Lake Stechlin. For the first application, a fast-response CTD 232 233 (conductivity, temperature and depth) profiler (XR-620 CTD+, RBR, Canada) was mounted onto a winch with a 30 m long water hose (4 mm inner diameter) attached. The CTD profiler 234 with hose was lowered down continuously at a constant speed (1 m min<sup>-1</sup>). The exact depth and 235 temperature of sampled water can be extracted from the CTD profiler by correcting for the 236 travel time of water sample flow in hose. For the spatial mapping, a GPS antenna (Taoglas, 237 AA.162, USA) was attached to the Picarro gas analyzer. The water intake was submerged 0.5 238 m below the water surface together with the CTD profiler and fixed to one side of the boat. The 239 boat was driven at a constant speed of 5 km h<sup>-1</sup>. 240

241 2.4 Theoretical background and data processing

The FaRAGE shares a similar working principle to the Weiss-type gas equilibrator
described by Johnson (1999). The theoretical background and equations are provided in S3.

A simplified calculation is described by referring to the manual headspace method. In principle the gas-water mixture is analogous to the static headspace method with the final  $CH_4$ gas concentration in the gas phase assumed to reach a full equilibrium with that dissolved in the aqueous phase. Therefore, by specifying the mixing ratio of air and water, the total mass of  $CH_{4_2}$ for instance, can be calculated by summing up the  $CH_4$  in the headspace with the dissolved  $CH_4$ (at equilibrium according to Henry's law, which is temperature and pressure dependent) in the aqueous phase and subtracting the mass of background CH<sub>4</sub> (from the carrying gas with known concentration). The dissolved CH<sub>4</sub>-gas\_concentration is then expressed as the volumetric concentration of the total net mass of either CH<sub>4</sub> or CO<sub>2</sub> in the dissolved phase in the given sample volume. A separated exemplary calculation sheet (excel file S5) is provided, which allows for correction for temperature and pressure change (Goldenfum, 2010).

As the equilibration is only partially reached (< 92%), a correction coefficient is needed. This can be obtained by measuring the water samples with known concentrations across a large gradient. By referring to the results measured with the manual headspace method assuming full equilibration (Magen et al., 2014), an equation for precise correction of the measured  $CH_4$ <u>dissolved gas (alsoand CO<sub>2</sub>)</u>-concentrations can be obtained.

## 260 **3 Results and Discussion**

## 261 **3.1 Detection limit, equilibration ratio and response time**

The FaRAGE is capable of achieving a high gas equilibration ratio. We observed a high 262 correlation ( $R^2 = 0.9991.000$ , p < 0.01) between the concentrations obtained using the 263 traditional headspace method and those measured using the FaRAGE (Fig. 2a) across a wide 264 range of dissolved CH<sub>4</sub> and CO<sub>2</sub> concentrations. The measurement accuracy is 0.5% (standard 265 deviation in relation to final concentration) once a stable plateau was reached (Fig. 2b2c). For 266 CH<sub>4</sub>, the FaRAGE reaches a high equilibration ratio (6362.6%) and ensures a rapid response. 267 The determined response time  $t_{95\%}$  is only  $12 \pm 1$  s when switching from low-to-high (nano-to-268 sub micro molar) dissolved CH<sub>4</sub> concentrations while the  $t_{95\%}$  is a little longer (15 ± 2 s) when 269 switching from high-to-low concentration (Fig.  $\frac{2b2c}{c}$ ). For the current design specifications that 270 271 allow for a high equilibration ratio, the detection is theoretically limited by the sensitivity of the coupled gas analyzer. In the lab tests, a clear response was observed at least for CH4 272 concentration at air saturation (16.95.5 nM inside the lab building). The measureable CH4 273

concentrations should be at least sub-nM ( $10^{-10}$  mol L<sup>-1</sup>) given the high performance of cavityring-down gas analyzers. This is more than sufficient for applications in inland waters where dissolved CH<sub>4</sub> concentrations are often above air saturation. <u>Despite CO<sub>2</sub> (Weiss, R. F., 1974)</u> is an order of magnitude more soluble in water than CH<sub>4</sub> (Wiesenburg and Guinasso, 1979), similar performances of the FaRAGE were observed when measuring dissolved CO<sub>2</sub>. An equilibration ratio of 67.1% (Fig. 2b) was achieved with a fast response (Fig. 2d; *t95%* = 10 ± 2 and 15 ± 2 for low-to-high and high-to-low, respectively) when a 2 m mixing tube was used.

The response time for the FaRAGE results from two components: 1) the response of the gas analyzer to changes in gas concentration and 2) the physical gas-water exchange process. The response time for the gas analyzer is 5 s when the CH<sub>4</sub> concentration increases (Fig. S2). The FaRAGE itself needs < 10 s to reach 95% of the final steady-state concentration.

Equilibration ratio and response time of the FaRAGE is not sensitive to the water-to-gas 285 mixing ratio (Fig. 2e3a) but rather to the length of the tube in installed attached after the gas-286 water mixing unit (Fig. 2d3c). Little-A small effect, of the increased water-to-gas mixing ratio 287 was also observed on the equilibration ratio in response to the increase of water-to-gas mixing 288 ratio. Also, tThe increase ofd water-to-gas mixing ratio did not significantly substantially 289 290 change the response time of the device (on average  $9.5 \pm 1.5$  s for low-to-high and  $13.9 \pm 2.4$  s 291 for high-to-low, respectively). This is in contrast to other types of equilibrators in which an 292 increase of water-to-gas mixing ratio was found to result in a faster response (Webb et al., 2016). 293 However, a sharp enhancement of equilibration ratio was observed due to the extended length of the tube for the gas-water mixing unit. A 91.8% equilibration ratio can be achieved by 294 295 extending the tube length to 13 m while extended response times are expected (low-to-high 17 296 s and high-to-low 47.5 s, respectively). The instabilityIncreases in response time were notable when the tube-length exceeded 13 m and were considered excessive at a tube length of 18 m 297 (Fig 3c-d). (abnormal sharp increase in response time) started from athe 13 m tube length (Fig. 298

3c-d) and became unacceptable when tube length isreached 18 m. Further enhancement of the 299 equilibration ratio was thus not possible when a longer tube (e.g. 18 m) was used. The gas flow 300 rate cannot be stabilized at 1 L min<sup>-1</sup> due to the increased resistance in response to the further 301 extension of tube length. Equilibration ratio and response time were affected by the length of 302 the tube after the gas-water mixing in a similar way as it was for CH<sub>4</sub> (Fig. 3b, d) with only one 303 exception in the response time when the dissolved CO<sub>2</sub> concentration changed from high to low. 304 The response time increased linearly ( $R^2 = 0.910$ , p < 0.01) from 11 s to 18 s in response to the 305 increase of water-to-gas ratio from 0.04 to 0.5. 306

As shown in Table S2 and Fig. S2, the fast response of the FaRAGE is partly due to the 307 extremely fast response of the Picarro Gas Scouter. This makes it unfair to compare with other 308 309 equilibrators in which different gas analyzers were used. Tests were performed by adapting the FaRAGE to two other greenhouse gas analyzers (Ultraportable Los Gatos and Picarro G2132-310 i) and the response times are listed in Table S3. Comparisons were made in Webb et al. (2016) 311 and Hartmann et al. (2018) where both CH<sub>4</sub> and <sup>13</sup> & C-CH<sub>4</sub> were measured using a Picarro 312 G2201-i (Picarro, USA). Here we used a similar Picarro stable isotopic gas analyzer (Picarro 313 314 G2132-i) and unified all previous reported response times  $\tau$  to t95% by applying the equation t95% =  $3\tau$ . The comparison between up-to-date previous studies and this study (Table S4) 315 316 demonstrated the extraordinary fast response relative to all existing gas equilibration devices. A 53 s response time was achieved when the FaRAGE was adapted to the Picarro G2132-i, 317 318 which is significantly substantially faster than others previously reported (171-6744 s).



329 reached.



Fig. 3 Factors affecting performance of the gas equilibrator for both dissolved CH4 and CO2. 331 (a)-(b) Equilibration ratio and response time in response to changing water/gas mixing ratio 332 (with a 2-m tube in the gas-water mixing unit). Black cross symbols are equilibration ratios, 333 and low-to-high and high-to-low response times are represented by red open and solid squares, 334 respectively. (c)-(d) Equilibration ratio and response time in response to changing tube length 335 336 of gas-water mixing unit (with a fixed water-to-gas mixing ratio of 0.5). Black cross symbols are equilibration ratios, and low-to-high and high-to-low response times are represented by red 337 open and solid squares, respectively. 338

# 339 **3.2 Depth profiles of dissolved CH**<sub>4</sub> and CO<sub>2</sub> from multiple lakes

340 Good agreement was observed between depths profiles of dissolved CH<sub>4</sub> and CO<sub>2</sub> 341 concentration measured using two different methods the FaRAGE and the manual headspace method (Fig. <u>34</u>). The observed The oOoccurrence of a maximum in the vertical profile of 342 343 dissolved CH<sub>4</sub> concentration in the upper layer of Lake Stechlin (Fig. 3b4a) is consistent with previous observations (Grossart et al., 2011; Tang et al., 2014; Hartmann et al., 2018). In Lake 344 Arend we also observed a CH<sub>4</sub> peak (Fig.  $\frac{3a4a}{a}$ ) although the overall concentration was lower. 345 346 The opposite was observed at Lake Großer Pälitz and Lake Zotzen (Fig. 4c) with an anoxic hypolimnion, where the dissolved CH<sub>4</sub> concentration was three orders of magnitude higher than 347 atin the epilimnion. Higher dissolved CO<sub>2</sub> ( $10^2 - 10^3 \mu M$ ) was also observed in the hypolimnion 348 of these two lakes (Fig. 4d) in comparison to the Lake Stechlin and Lake Arend (<  $10^2 \mu M$  in 349 350 Fig. 4b).

In contrast, with to the headspace method, the FaRAGE allowed for the localized profiles 351 of CH<sub>4</sub> and CO<sub>2</sub> concentration maximum to be described at a high vertical resolution, similar 352 to that obtained with more sophisticated membrane filter equilibrators (Hartmann et al., 2018; 353 Gonzalez-Valencia et al., 2014). The FaRAGE was capable of resolving differences in 354 dissolved CH<sub>4</sub> and CO<sub>2</sub> concentrations in lake water at decimeter scales-resolution with ease. 355 Whilst care should be taken to ensure the sampling hose moves smoothly and slowly through 356 the water column, continuous profiling of a 20 m deep lake can be completed in 30 min. This 357 358 is a big advantage since in situ CH4 concentrations can vary at very short time scales (hours to 359 days) subject to internal production, oxidation, weather conditions, and etc. (cf. Hartmann et al. (2020)).360



Fig. <u>4</u> Depth profiles of dissolved CH<sub>4</sub> and CO<sub>2</sub> concentration from <u>a set of lakes in Germany</u>:
(a)-(b) Lake Stechlin and Lake Arend with an oxygenated hypolimnion in summer; (c)-(d) Lake
Großer Pälitz and Lake Zotzen, both with an anoxic hypolimnion in October. Note the log
transformed x-axis is used in (c)-(d). References using the headspace method are designated as
red open circles and measurements using the FaRAGE are shown as solid lines.

368 **3.3 Resolving spatial variabilities variability** of dissolved CH<sub>4</sub> and CO<sub>2</sub> concentrations

We confirmed the capability of the FaRAGE to operate continuously over a 7-h period 369 without notable decreases in performance (Fig. 4a5a-b). Benefitting from its fast response rate, 370 surface water dissolved CH<sub>4</sub> and CO<sub>2</sub> concentrations across the 4.52 km<sup>2</sup> Lake Stechlin was 371 were mapped with great detail within one day (Fig. 5c-d). During the cruise, 10 reference 372 373 measurements were made at different sites and times, which were consistent with nonstop online in situ measurements. The cruising survey demonstrated the capability of this device for 374 resolving not just vertical dynamics of CH<sub>4</sub> and CO<sub>2</sub> in lake water, but also the potential for 375 studying horizontal gas distributions of CH4-across large distances, for instance large lakes and 376 rivers. With a driving speed of 5 km  $h^{-1}$  and a response time of 12 s, a spatial resolution of 17 377 378 m can be achieved, which is sufficient for such a medium-sized lake. The relative higher dissolved CH4 concentrations in the shallow littoral zone of Lake Stechlin (Fig. 4b) reflect 379 higher CH<sub>4</sub> release from the local sediment. 380

381



382

**Fig. 5** Map of surface dissolved CH<sub>4</sub> concentration at Lake Stechlin. (a)-(b) Time series of 7-h continuous surface water CH<sub>4</sub> and CO<sub>2</sub> measurement on March 28, 2019. The reference headspace measurements are shown as red circles. (c)-(d) Spatial distribution of surface water CH<sub>4</sub> and CO<sub>2</sub> concentration is given on top of the lake's bathymetry. Colored symbols show CH<sub>4</sub> and CO<sub>2</sub> concentrations according to the color bars. Black lines show the outline of the lake with depth contours.

# 389 4 Comments and Recommendations

# 390 4.1 Adaptability to different gas analyzers

391 The reasons for the significantly substantially shortened response time of the FaRAGE 392 compared to other types of gas equilibrators are two-fold. While the working principle of the FaRAGE is based on the bubble-type (Schneider et al., 1992) and Weiss-type equilibrators 393 (Johnson, 1999), a reduced headspace volume is adopted, which enhances the physical gas-394 water exchange. Another reason is the use of an extremely fast-response gas analyzer (Picarro 395 Gas Scouter 4301). It is a highly recommended combination for concentration-measurement of 396 397 dissolved gasses when the best time-wise performance is preferred due to its great mobility (Table S2). However, coupling to other Cavity-Ring-Down gas analyzers is also possible (Table 398 399 S3). This feature enables a possibility to investigate stable isotopic nature of dissolved CH4 and 400 CO<sub>2</sub>, which is important when sources of CH<sub>4</sub> and CO<sub>2</sub> need to be identified.

When a portable gas analyzer (Picarro Gas Scouter or Ultraportable Los Gatos) is used 401 402 for measuring CH<sub>4</sub> and CO<sub>2</sub> concentrations only, the gas equilibrator can be optimized for different application environments. The length of coiled tube for gas-water mixing can be 403 404 adjusted to change the response time (Fig. 2d3c-d). For smaller lakes a higher spatial resolution can be obtained by shortening the equilibration tubing, which shortens the response time, and 405 406 hence increases the spatial resolution, whilst maintaining an acceptable equilibration ratio (51% 407 when tube length is 1 m). In environments with extremely low dissolved CH<sub>4</sub> concentrations, e.g. ocean waters, a longer gas-water mixing tube should be used to ensure a high gas 408 equilibration ratio. 409

To measure stable isotopic CH<sub>4</sub> and CO<sub>2</sub> in water, the sensitivity of the FaRAGE can be modified to better adapt to the choice of gas analyzer (e.g., when Picarro G2201 i or G2132 i is used). For example, high dissolved CH<sub>4</sub> concentrations (e.g.  $\mu$ M-to-mM range) can be measured with greater accuracy by increasing the flow rate of the carrier gas relative to the sample water flow, therefore diluting the CH<sub>4</sub> concentrations to the range of the gas analyzer. This can be particularly useful, for instance, when an instrument has an optimal precision at a low concentration range (1.8-12 ppm, for e.g., Picarro G2201-i or G2132-i analyzersPicarro isotopic gas analyzer) for <sup>13</sup> &C-CH4 measurements. By using pure N<sub>2</sub> gas or carrier gases (e.g. Helium and Argon) and corresponding gas analyzers, it would be possible to measure other dissolved trace gas concentrations, e.g.  $CO_2$ -can be measured simultaneously ( $CO_2$ -was tested in this study, but not shown for simplicity)N<sub>2</sub>O. In addition, benefited <u>due to</u>from the high equilibration ratio of this device (max. 91.8%), it would be possible to measure dissolved CH4 (and other gases) close to equilibrium concentrations.

## 423 **4.2** Uncertainties due to suspended solids, temperature and pressure change

The FaRAGE is proven to be resistant to suspended solids in freshwater lakes without 424 having to use additional accessories. As shown in Fig. S3, apparent phytoplankton blooms were 425 426 observed in the two studied lakes each with a high biomass (Chl- $a > 30 \mu g L^{-1}$ ) in the epilimnetic 427 water. The measurements were unaffected, without any interruptions during measurements. As 428 algal particles are a large component of suspended particle concentration in freshwater elearwater-lakes without a high suspended sediment load concentration systems, it is safe to 429 430 claim the resistance of this device to suspended solids in such a-systems. However, care must be taken to avoid the water intake hose hitting the bottom sediment, which could cause blockage 431 432 of the water hose. An additional filtration unit for the water intake might be needed when the device is to be applied to turbid rivers. 433

The temperature and hydrostatic pressure could both change when water is pumped out through a water hose. To consider the temperature effect, a fast temperature logger is used (Fig. 1) which allows for corrections in calculation. Instead of using *in situ* lake temperature, the temperature measured at the gas equilibrator, should be used where gas equilibration occurs, should be used. Our measurements found a minor effect when measuring surface waters but an apparent warming for hypolimnetic water in deep lakes (Fig. S4). While a calibration can be 440 done directly by taking water samples from multiple depths of the lake (e.g., Fig. 3) to consider
441 this effect, one could make the calculation without taking many samples by applying
442 temperature correction.

The temperature correction can be made by referring to the manual headspace method. 443 444 The constant gas and water flow can be used as headspace and water volume, respectively. By 445 considering the temperature and pressure effects on gas solubility, the dissolved CH<sub>4</sub> and CO<sub>2</sub> concentrations can be calculated (an example calculation sheet is provided in Table S5). The 446 447 calibration curve can be established using the manual headspace measurements as standards. The final concentrations can be corrected for partial equilibration by applying the equation from 448 the calibration curve (e.g., Fig. 2a-b). The response time should be deduced when calculating 449 450 CH<sub>4</sub> and CO<sub>2</sub> depth profiles and spatial distributions, in addition to the time lag caused by 451 pumping water samples by using an extended water intake hose.

#### 452 **4.3 Calibration, maintenance and mobility**

The FaRAGE can be readily adopted for measuring other trace gases when coupled with 453 454 other portable gas analyzers. Due to differences in gas solubility (Duan and Sun, 2003; Wiesenburg and Guinasso Jr, 1979), for each new gas, it would be necessary to establish the 455 relative equilibration efficiency and response time, following the approach we outlined here for 456 CH<sub>4</sub> and CO<sub>2</sub>. Once set, a new calibration is only required when the tubing diameter or length 457 is changed (when the old one is filthy no longer usable due to biofilm growth). This can be done 458 by referring to a number of known concentrations that covers a wide range (at least 5), e.g., 459 460 taking water samples from different water depth of the lake or a gradient from littoral to pelagic zones. Once this full calibration is made, the calibration curve can be used for calculating the 461 subsequent measurements. A one-point reference measurement should be performed between 462 depth profiles or transects to check for apparent drifting. This can usually be done by taking 463 one surface water sample from a lake for manual headspace measurement. Care should be taken 464

when measuring in lakes with an anoxic hypolimnion where hydrogen sulfide is likely to accumulate. The performance of Cavity-Ring-Down gas analyzers can be potentially affected by organics, ammonia, ethane, ethylene, or sulfur containing compounds<u>H2S gas</u> (Kohl et al., 2019). At these sites, it is always recommended to take additional samples and measure them with traditional methods (e.g., with a Gas Chromatograph Analyzer). it is recommended to use a copper scrubber to remove H2S from the gas samples (Malowany et al. 2015) and no time delay will be induced.

The gas equilibrator should be carefully maintained. Replacement of parts is recommended at a monthly basis provided the device is heavily in use. They include bubble diffusor and the coiled gas-water mixing tube. In addition, to ensure the performance and prevent biofilm formation the gas-water mixing and separation units should be cleaned after use. Running with distilled or Milli-Q water would help to rinse the device and reduce the risk of biofilm development in the inner tubes. The performance of peristaltic pumps should be also regularly checked and the inner pump tubes need to be replaced to ensure a constant water flow.

The combination of FaRAGE with the Picarro Gas Scouter provides the most mobility. The system can be easily carried by one person and work in a small aluminum or inflatable boat with where a maximum capacity of three people is possible. The device can also work in bad weather with additional measures based on protecting the gas analyzer from water damage by rain or flooding.

- 484 **Code availability**
- 485 Not applicable.

## 486 Data Availability

An example calculation sheet (raw data of Fig. 2a) is provided as part of supporting
information for device calibration and for temperature and pressure correction when calculating

489 dissolved methane concentration. The full data sets associated with lab and field tests are490 available upon request.

## 491 Supplement link

492 From Copernicus.

## 493 Author contributions

494 SBX and WW proposed the idea and built the first prototype. LL improved the prototype 495 and conducted lab and field tests. JW contributed to the field tests. AL contributed to the 496 derivation of equations; HPG <u>led the project and advised the development of the modified</u> 497 prototype. LL drafted the initial manuscript. All authors discussed the results and commented 498 on the manuscript.

## 499 Competing interests

500 The authors declare that they have no conflict of interest.

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1	Supporting Information for
2	A Fast-response automated gas equilibrator (FaRAGE) for continuous in situ
3	measurement of methane <u>CH4 and CO2</u> dissolved in water
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### 21 S1. Details of parts, gas analyzers and costs

22 To make the FaRAGE field deployable, parts were tightly packed into an aluminum box with a built-in power supply. The electric parts were separated from other parts containing 23 water in the box by using a plastic board. Ports were well labelled on the right-handed side so 24 25 that even somebody new to the system can work with it. To help interested readers rebuild the device, the two key components (gas-water mixing unit and gas-water separation unit) were 26 shown in the detailed technical drawings (Fig. S1). The suppliers and costs for these parts 27 28 were listed in Table S1. A total of 3,560 € was calculated for building the complete device excluding the costs for the power supply. As the expensive RBR temperature logger is not a 29 necessity since we happen to have it in storage, a cheaper temperature logger can always be 30 used. For example, a fast HOBO temperature logger (HOBO U12 with a Temperature probe 31 TMC1-HD) is available for  $< 200 \in$ . The total cost can be cut down significantly to  $< 3,000 \in$ . 32

The FaRAGE is capable of couplinge with different greenhouse gas analyzers, depending 33 on the research question and instrument availability. Three most widely used field-deployable 34 gas analyzers were compared in Table S2 to provide a reference for readers when choosing a 35 gas analyzer. They are GasScouter G4301 (Picarro, USA), Ultraportable Greenhouse Gas 36 37 Analyzer (Model 915-0011, LosGatos Research, USA) and Picarro G2132-i isotope analyzer (Picarro, USA). We noticed Picarro 2201-i has been more often used, but our Picarro G2132-i 38 39 is an equivalent instrument except that the module for isotopic CO<sub>2</sub> is not installed. The former two instruments measure CH<sub>4</sub>, CO<sub>2</sub> and H<sub>2</sub>O and the last one additionally measures 40 stable isotopic CH<sub>4</sub>. As shown in Table 2, clearly GasScouter G4301 is most suitable for field 41 42 measurement of dissolved CH<sub>4</sub> concentrations due to its extremely high mobility. The built-in 43 battery pack can support 8 h continuous measurements and the ability to amount GPS antenna offers the advantage in doing spatially-resolved measurements. The Picarro G2132-i isotope 44 analyzer is most immobile because of it is heavy and relative high power consumption in 45

addition to its particularly long time to warm up (30 min). However, Picarro G2132-i
measures stable isotopic CH<sub>4</sub>, while the other two instruments cannot. Care must be taken and
a proper boat with stable power supply is needed in order to use Picarro G2132-i as a coupling
unit for the FaRAGE.



S3

50

Fig. S1 Assembled-Technical drawings of FaRAGE key components. in an aluminum box
with built in power supply. Main parts and ports are marked on the figure. The power supply
is made from a 100 Ah (12 V) Li ion battery coupled with a power transformer that converts
12 V DC power to 230 V AC power.(a) Gas-water mixing unit and (b) gas-water separation
unit. Note: ID and OD are the abbreviations of inner diameter and outside diameter,
respectively.

Items	Dimensions	Model specifications	Producer/Supplier	Quantity	Cost
Diving tank	10 L	Pressure up to 230 bar	Atlantis Berlin	1	199€
Pressure regulator		200 bar / 0 - 10 bar, HERCULES CK1401	Gase Dopp	1	59.98€
Mass flow controller (for air)		SIERRA Model C50L SMART-TRAK	SCHWING Verfahrenstechnik GmbH	1	995€
Flow meter (for water)		0.082-0.82 L min-1, 1355GAF3CBXN1AAA	Brooks Instrument GmbH	1	943.91 €
Peristaltic pump	9 x 11 x 16 cm	0-500 mL min-1, 24V/1A DC power	Purchased from Taobao, China	2	200€
Temperature logger		Precision 0.001 °C, maximum 6 Hz measurement frequency, TR-1050	RBR, Canada	1	1,000€
Tygon tube	3.2/6.4 mm in./out. Ø	Saint-Gobain Schlauch Tygon S3 E-3603 2.5bar	RS Components GmbH	15 m	68.78€
Plastic syringe for mixing unit	5 mL	Cut to 3 mL, sealed with a rubber stopper	BD plastipak	1	1€
Plastic syringe separation unit	30 mL	Sealed with a rubber stopper	BD plastipak	1	1€
Plastic syringe for desiccant	50 mL	Filled with silicone beads, sealed with a rubber stopper	BD plastipak	1	1€
Rain pipe			Toom	1	10€
Bubble diffusor	12 mm Ø, 16 mm length	Pawfly 0.6 Inch Air Stone, UL266	Ebay	1	1€
Teflon membrane filter	25 mm Ø	PTFE 0.2 μm	Lab Logistics Group GmbH	2	2€
Tube connector	for 3.2-4.2 mm	LL male, barbed hose connection: PP, 10 pcs/pack   2- 1882	neoLab Migge GmbH	10	12€
Aluminium box	38.3 x 57 x 37.5 cm	65 L, Stier aluminium box	Amazon	1	64.95€
Total					3,560€

57 **Table S1.** List of materials for parts of the FaRAGE prototype. Details on dimensions, model, producer/supplier and cost are provided.

Analyzer	Gases	Gas flow rate	Cavity pressure	Measurement frequency	Concentration range	Precision	Response time	Dimensions	Weight	Power consumption	GPS Kit	Mobility
GasScouter G4301	$CH_4$ $CO_2$ $H_2O$	1 L min <sup>-1</sup>	> 700 Torr	1 Hz	CH₄: 0-800 ppm CO₂: 0-3% H₂O: < 3%	CH <sub>4</sub> : 3 ppb CO <sub>2</sub> : 0.4 ppm	5 s	35.6 × 17.7 × 46.4 cm	10.4 kg	25 W, built-in Li-ion battery	Yes	Very high
Ultraportable Greenhouse Gas Analyzer 915–0011	$CH_4$ $CO_2$ $H_2O$	0.5 L min <sup>-1</sup>	140 Torr	1 Hz	CH <sub>4</sub> : 0.01-100 ppm CO <sub>2</sub> : 1-2% H <sub>2</sub> O: < 7%	CH₄: 2 ppb CO₂: 0.6 ppm	~10 s	17.8 x 47 × 35.6 cm	17 kg	70 W, on battery/AC power	No	High
Picarro G2132-i	$CH_4$ $\delta^{13}C-$ $CH_4$ $CO_2$ $H_2O$	25 mL min <sup>-1</sup>	148 Torr	0.5 Hz	CH <sub>4</sub> : 1.8-10 ppm high- performance mode; 10-1000 high-range mode CO <sub>2</sub> : 200 - 2000 ppm guaranteed range H <sub>2</sub> O: <2.4 % guaranteed range	$CH_4$ : 5 ppb + 0.05 % of reading (12C); 1 ppb + 0.05 % of reading (13C) $CO_2$ : 1 ppm + 0.25 % of reading (12C)	~30 s	43.2 x 17.8 x 44.6 cm	27.4 kg	205 W, AC power	No	Fair
Note: 1) GasScouter G4301 does not use a vacuum pump to maintain a stable cavity pressure and the gas flow rate should be stable but slightly above/below the recommended value.												
2) All gas analyzers are sensitive to liquid-phase water, therefore a hydrophobic filter is normally placed before the gas intake to protect												
instru 3) Accor	ment fro	om bei Picarr	ng floode	d.	ur for concentrations of	H2O and CO2 w	rell above 1	normal ambi	ent leve	ls. as well as	other	

58	Table S2.	Summary	of technical	details for the	three greenhouse	gas analyzer	s tested in this study	′.
					0		2	

64 organics, ammonia, ethane, ethylene, or sulfur containing compounds.

#### 65 S2. Re-evaluation of response time of gas analyzers

66 While response time for each gas analyzer has been provided by its manufacturer (Table 67 S2), a large difference was found when they were re-evaluated (Fig. S2). Picarro GasScouter 68 has the fastest response to concentration increase, in comparison to four-fold and eight-fold 69 slower response for portable Los Gatos and Picarro G2132-i, respectively. All three gas 70 analyzers were seen longer response time when concentration changed from high to low. The 71 Picarro GasScouter still has the best performance compared to the other two.





**Fig. S2** Response times of gas analyzers. Triplicated measurements were performed. Low-tohigh and high-to-low concentration changes were investigated. The response time was determined by taking the time when 95% of final concentration was reached. For  $\delta^{13}$ C-CH<sub>4</sub>, 30 s moving average data was used.

## 77 S3. Theoretical background

With the present design of the **Fast-Response Automated Gas Equilibrator (FaRAGE)**, a continuous dynamic gas-water mixing occurs and the carrier gas is partially equilibrating with the CH<sub>4</sub> dissolved in water sample. The gas composition reaching the gas analyzer depends on equilibration time and flow rates. The equilibration between the carrier gas and the water sample during flowing through the FaRAGE depends on the concentration difference between the gas stream (*C* in µmol L<sup>-1</sup>) and the dissolved (aqueous) concentration in the sample water (*C<sub>a</sub>*):

85 
$$\frac{dC}{dt} = k \times \left(\frac{1}{HRT}C_a - C\right) \tag{1}$$

86 Where *H* is the temperature-dependent Henry constant (mol L<sup>-1</sup> atm<sup>-1</sup>), *R* the universal 87 gas constant (8.31 J mol<sup>-1</sup> K<sup>-1</sup>), *T* is temperature (K) and *k* (s<sup>-1</sup>) is an exchange coefficient. The 88 equilibrium gaseous concentration  $C_{eq} = \frac{1}{HRT}C_a$  corresponds to the headspace concentration 89 of a fully equilibrated water sample. *k* is expected to depend on the relative flow rates of gas 89 and water as well as on the flow regime and mixing of both phases in the FaRAGE. For an 89 initial concentration of CH<sub>4</sub> in the carrier gas *C<sub>ini</sub>*, the time-dependent concentration during the 89 passage through the equilibrator is:

93 
$$C(t) = (C_{ini} - C_{eq})e^{-kt} + C_{eq}$$
 (2)

94 After a device-specific partial equilibration time  $t_e$ , the CH<sub>4</sub> concentration in the carrier 95 gas has changed to  $C_{pe}$ , which is measured by the gas analyzer

$$C_{pe} = C(t_e) = K(C_{ini} - C_{eq}) + C_{eq}$$
(3)

96

97 With  $K = e^{-kt_e}$  being a device-specific coefficient, which can be obtained by calibrating 98 the FaRAGE with at least one water sample of known dissolved concentration ( $C_{eq}$ ) through:

99 
$$K = \frac{C_{pe} - C_{eq}}{C_{ini} - C_{eq}}$$
(4)

100 The equilibrium headspace concentration of CH<sub>4</sub> in the water sample and the 101 corresponding dissolved concentration can be estimated from the initial and final carrier gas 102 concentration as:

103 
$$C_{eq} = \frac{1}{HRT} C_a = (KC_{ini} - C_{pe})/(K-1)$$
(5)

For a high flow rate of the carrier gas, the response time of the system to changing dissolved concentrations at the sample intake is predominantly determined by the gas venting rate, i.e. by the total volume of carrier gas that is in contact with the water sample, divided by the volumetric gas flow rate (cf. level two model of Johnson (1999)), as well as by the response time of the gas analyzer.

**Table S3.** Response times when adapting to different gas analyzers. Tests were performedwith a water/gas mixing ratio of 0.5. Triplicates were made and mean values are shown here.

	<b>T</b>	t <sub>95%</sub> response time (s)			
Gas analyzer	Treatment	CH₄	CO <sub>2</sub>	<sup>13</sup> <i>∂</i> C-CH4	
Cas Secutor C4201	Low-to-high	13	6	-	
Gas scouler G4301	High-to-low	13	6	-	
Ultraportable	Low-to-high	34	32.3	_	
Greenhouse Gas Analyzer 915-0011	High-to-low	37	30	-	
	Low-to-high	53	53	53	
Picarro G2132-I	High-to-low	65.3	60.7	65.3	

111 Note: Response time for Picarro G2132-i was determined without using a desiccant. Repeated 112 tests were done to examine the effect of desiccant. The response time was extended by 150 s 113 when the 20 mL desiccant was used. A desiccant should be used to keep the moisture content 114 in gas samples < 1%. Drierite and magnesium perchlorate (Mg(ClO<sub>4</sub>)<sub>2</sub>) are recommended for 115 such a purpose due to their high performance. It was shown by Webb et al. (2016) that both 116 types of dryer had no effect on CH<sub>4</sub> and CO<sub>2</sub>, except for a 1.5 min delay in response time for 117 CO<sub>2</sub> when using Drierite.

**Table S4.** Comparison of response times for simultaneous measurement of dissolved CH<sub>4</sub> and  $\delta^{13}$ C-CH<sub>4</sub> in water from previous studies using different devices (after Webb et al., 2016, Hartman et al., 2018) compared with response times in this study. Response time was unified here to *t*95% to allow for meaningful comparison. The *t*95% values were taken from literature by applying *t*95% = 3 $\tau$  and the mean were used.

Device	t <sub>95%</sub> response time (s)	Study
Weiss-type (small)	6744	Li et al. (2015)
General oceanics	6123	Webb et al. (2016)
Shower head	4971	Webb et al. (2016)
Weiss-type (large)	3600	Rhee et al. (2009)
Marble	2679	Webb et al. (2016)
Bubble-type	2034	Gülzow et al. (2011)
Liqui-Cel (medium)	1251	Webb et al. (2016)
Liqui-Cel (small)	531	Webb et al. (2016)
Liqui-Cel (large)	351	Webb et al. (2016)
Liqui-Cel (small) in vacuum mode	171	Hartmann et al. (2018)
Combined Weiss-type with bubble-type	53	This study

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# 124 S4. The depth profiles of phytoplankton biomass at Lake Arend and Lake Stechlin

As in most freshwater lakes phytoplankton is a large component of suspended solids in water column, the effect of phytoplankton biomass on the performance of the gas equilibrator was evaluated. Fig. S3 shows that the presence of in both study lakes high phytoplankton
biomass (represented by Chl-a) within the surface 20 m water depth in the both study lakes.





Fig. S3 Depth profiles of Chlorophyll-a (Chl-a) at Lake Arend and Lake Stechlin on June 17
and July 23, 2019 with (b)-(c) dissolved CH<sub>4</sub> and CO<sub>2</sub> profiles. The profiles were measured
using a BBE FluoroProbe (Moldaenke, Germany) simultaneously with dissolved gas profiles.

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Fig. S4 An example of altered depth profile of water temperature at Lake Stechlin in autumn
2019. (a) Comparison of in situ water temperature (red line) with water temperature measured
in the FaRAGE (black line). (b) The difference between the two temperature measurements
(In FaRAGE - In situ).

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