Interactive comment on "Mobile open dynamic chamber measurement of methane macroseeps in lakes" by Frederic Thalasso et al.

Anonymous Referee #1 Received and published: 13 October 2020

This ms covers at least four important research issues on greenhouse gases (GHG) in freshwater systems:

1. Seepages in freshwater lake's sediments 2. Estimation of emissions in systems with unevenly distributed hotspots 3. Development of an easy-to-use instrument with high precision in a wide concentration range 4. Measurements in remote areas

The development and successful use of a newly developed flux chamber is in the center of the paper by F. Thalasso et al., the so-called Mobile open dynamic chamber (MOD). A permanent flow of gas makes the chamber to an open system, the gas of interest (CH4, CO2) is emitted across the air-water-interface (AWI) into a cavity, from where it is transported by the continuous flow of ambient air to the GHGanalyser (no matter of which brand). The chamber can be connected to a boat manned or unmanned and moved along a system of transects across the interesting area of an aquatic system, e.g. a lake with seeps. The authors represent a set of equations to calculate the emission rates for systems based on data generated by MOD, as well as assembly instructions for the chamber. The ms will allow interested scientists to build and use a MOD and further on, to calculate gas emissions. This easy-to build design and the abandonment of special gases in tanks allow usage in remote places, like the tested Alaskan lake. For test and calibration purposes, a second lake in Mexico as well as a very specific gas trap were involved. While L. Guadalupe represents another system with low or medium ebullition rates, the tested trap is unique, already by its trapping area of 45 m². It is interesting that the results fit between MOD and "giant trap", for the idea of using simple repeatable techniques with low man power in a remote area, a few simple inverted funnels would have been more useful. As mentioned by the authors, new small and reasonable sensors (CH4 and CO2) become more and more available and could replace expensive gas-analysers soon. I can imagine that in near future slightly modified MODs equipped with sensors and data-storages and connected to remote vehicles will help to solve the problem of spatial and temporal resolution of emission rates from freshwater lakes.

<u>Our answer</u>: Thank you for the positive appreciation of our work. We are pleased that Anonymous Referee #1 found our manuscript of interest.

Technical comment: "Following equations S4-6 (supporting information) the authors calculate the spherical diameter of gas bubbles rising to the AWI, based on the methane content in bubbles. This content has to be analysed in parallel (here by gas chromatography). From my point of view these calculation simplifies the bubble size calculation and additionally, as it is known that GHG content within bubbles can vary by several per cent, another unknown is in the equation. Perhaps I oversee it,

but I am missing water depth/pressure at depth in these equations as well as size when leaving the sediment. I recommend to rewrite this paragraph to clarify the calculation pathway".

<u>Our answer</u>: We agree that pressure should be specified in our calculations. We have clarified this section of the supporting information as follows;

"From M_B , the volume of the bubbles (V_B) and their equivalent spherical diameter (d_B) at atmospheric pressure were determined, assuming that the CH₄ content in the bubbles ($%_{CH4}$) is known, according to Eq. (S5) and (S6), respectively.

$$V_B = \frac{M_B}{16} \cdot \frac{R \cdot T}{P} \cdot \frac{1}{\%_{CH4}} \tag{S5}$$

$$d_B = 2 \cdot \sqrt[3]{\frac{3 \cdot V_B}{4 \cdot \pi}} \tag{S6}$$

where 16 is the molecular weight of CH₄ (g), *R* is the universal gas constant (L atm mol⁻¹ K⁻¹), *T* is the temperature (K) and *P* is the atmospheric pressure (atm).

Since bubble volume and diameters are important for mass transfer determination during their migration to the lake surface, the actual bubble volume (V'_B) at a given depth (D) within the water column is given by Eq. (S7).

$$V'_{B} = V_{B} \cdot \frac{P}{\frac{(\rho \cdot g \cdot D)}{101,325} + P}$$
(S7)

where ρ is the water volumetric mass density (kg m⁻³), g is the standard gravity (m s⁻²), and 101,325 is the conversion factor from Pa to atm.

Interactive comment on "Mobile open dynamic chamber measurement of methane macroseeps in lakes" by Frederic Thalasso et al.

Anonymous Referee #2 Received and published: 19 October 2020

The manuscript introduces a mobile open dynamic chamber to determine the methane flux from lakes, ebullitive or diffusive. The Ms is well written and is clear and concise. However, there are some aspect which I found difficult to follow:

Our answer: Thank you for this kind appreciation of our work.

The design of the MOD is a bit difficult to grasp. More photos could be helpful here. Figure 1 should be improved, why is the top of the chamber open? What sort of purge ventil is used?

<u>Our answer</u>: We appreciate this comment. It is important to ensure the reader clearly understands the MOD chamber design. We attended this comment by including an additional cross-section in Figure 1, which indicates that the chamber is closed in its upper part. We also included two more pictures of the chamber in the supporting information, as new Figure S3. Please note that the purge design is described around L190.

I found the indices for the different parameters a bit confusing. D- for detector and C for chamber, ok, but I and O ??

<u>Our answer</u>: Thank you for this comment, we agree. We changed subscript i for P (standing for purge) and subscript 0 to B (standing for bubbles/ebullition). We also included a new Table of notation in supporting information. We hope this is clearer now.

I was wondering, when the detector is sucking gas from the chamber and there is no ebullition, the purge ventil would let air into the chamber. I do not understand how you correct for this dilution and how you realize when there is more ebullition or more dilution? Ok, I read now the details on the purge ventil. But still, did you correct your measured data for a possible dilution?

<u>Our answer</u>: Yes indeed, our mass balance equations consider the flow rate that is entering the chamber when ebullition is low (Eq. 4). However, we also indicate that the input of CH_4 through the purge is negligible, compared to the CH4 emitted by the lake (Eq. 5 and text related).

Why did you divide your measurements into segments? The nice thing about your MOD is that you have continuous measurements on the whole lake...

<u>Our answer</u>: This is correct, we divided our transects into segments, and for each of them we determined a mean emission. The main reason for this approach is the stochastic nature of ebullitive events, generating instantaneous flux varying several orders of magnitude in matter of seconds (Figure 5 and new Figure S5). The interpolation of instantaneous fluxes would be extremely difficult to perform and, in our opinion, of moderate interest as being a representation of a very specific instant. On the contrary, the mean emission measured during each segment (typically 10 m long), gives the mean emission in the corresponding region of the lake that can be easily interpolated.

Some more examples for the measured data and calculated fluxes would be appreciated.

<u>Our answer</u>: We agree. We have included a second example of measurement observed during a transect, presented in Supporting information as new Figure S5.

New text included (in red):

Figure 1: Conceptual sketch of the mobile open dynamic (MOD) chamber, shown at the surface of the lake, passing over an intense seep (A); Cross section of the chamber cavity (B). Darker and lighter blue colors indicate three aluminum sheets welded together.

Figure S3. Superior (A) and inferior (B) view of the chamber hull with lateral floats added for improved stability.

Figure S5. Additional example of; (A) C_D (grey solid line) and C_C (black solid line) measured during a transect, and (B) instantaneous flux computed from these concentrations. Blue arrows show when large bubbles were captured by the chamber. Please note the logarithmic scales.

Marked manuscript: Mobile open dynamic chamber measurement of methane macroseeps in lakes

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Abstract. Methane (CH₄) seepage; i.e., steady or episodic flow of gaseous hydrocarbons from subsurface reservoirs, has been identified as a significant source of atmospheric CH₄. However, radiocarbon data from polar ice cores recently brought into question the magnitude of fossil CH₄ seepage naturally occurring. In northern high latitudes, seepage of subsurface CH₄ is impeded by permafrost and glaciers, which are under an increasing risk of thawing and melting in a globally warming

- 15 world, implying the potential release of large stores of CH_4 in the future. Resolution of these important questions requires a better constraint and monitoring of actual emissions from seepage areas. The measurement of these seeps is challenging, particularly in aquatic environments, because they involve large and irregular gas flowrates, unevenly distributed both spatially and temporally. Large macroseeps are particularly difficult to measure due to a lack of lightweight, inexpensive methods that can be deployed in remote Arctic environments. Here, we report the use of a mobile chamber for measuring
- 20 emissions at the surface of ice-free lakes subject to intense CH₄ macroseepage. Tested in a remote Alaskan lake, the method was validated for the measurement of fossil CH₄ emissions of up to 1.08×10^4 g CH₄ m⁻² d⁻¹ (13.0 L m⁻² min⁻¹ of 83.4 % CH₄ bubbles), which is within the range of global fossil methane seepage and several orders of magnitude above standard ecological emissions from lakes. In addition, this method allows for low diffusive flux measurements. Thus, the mobile chamber approach presented here covers the entire magnitude range of CH₄ emissions currently identified, from those
- standardly observed in lakes to intense macroseeps, with a single apparatus of moderate cost.

1 Introduction

Methane (CH₄) is a powerful greenhouse gas, that contributes about 20 % of the warming induced by greenhouse gases (Kirschke et al., 2013), with a global emission estimated to 572 or 737 Tg CH₄ yr⁻¹, for top-down or bottom-up budget estimations, respectively (Saunois et al., 2020). In addition to biotic and industrial sources, gas seepage; i.e., steady or

30 episodic flow of gaseous hydrocarbons from subsurface sources to the surface, has been identified as a significant source of atmospheric CH₄, estimated to range 42–76 Tg CH₄ yr⁻¹ (Schwietzke et al., 2016; Etiope et al., 2019). However, recent

analysis of atmospheric CH₄ radiocarbon ages in polar ice cores suggests that fossil CH₄ seepage of natural origin is at least an order of magnitude lower (Hmiel et al., 2020). Thus, CH₄ seepage, which has been classified into microseepage and macroseepage (i.e., diffuse exhalation and channeled flows, respectively), and previously thought to be a major component

- 35 of the global CH₄ cycle, needs to be better constrained.
- In northern latitudes, large quantities of geologic CH₄ are trapped by permafrost and glaciers, which form a "cryosphere cap" that restricts their flow to the atmosphere. Given that the Arctic is exposed to greater climatic warming than other latitudes (Trenberth et al., 2007; Post et al., 2019; Ito et al., 2020), the disintegration of the cryosphere cap would lead to transient release of CH₄ along faults (Spulber et al., 2010), through glacier retreat (Lamarche-Gagnon et al., 2019) and/or through
- 40 permafrost thawing (Walter Anthony et al., 2012). The magnitude of that potential CH₄ release is unknown, but a carbon store of over 1,200 Pg trapped by the cryosphere cap has been estimated (Isaksen et al., 2001; Flores et al., 2004; Gautier et al., 2009; McGuire et al., 2009; Collett et al., 2011). Hence, the conversion and release of a small fraction of that carbon to CH₄ may represent a significant input to the current atmospheric CH₄ pool, estimated to 5 Pg (Isaksen et al., 2001; Engram et al., 2020).
- 45 It is therefore of utmost importance to locate and accurately quantify CH₄ seepage. In aquatic environments, the location of CH₄ seepage can be determined by direct gas measurements or through visual observation of ebullition; i.e., outburst of gas. In northern latitudes, seasonal ice cover provides an unique opportunity to more accurately assess CH₄ ebullition, since the physical impact of bubbles breaking at the water surface delays ice formation, resulting in bubble-induced open holes during early winter (Walter Anthony et al., 2012). Later during the winter, ebullition also results in heterogeneous ice cover with
- 50 gas inclusions that can be detected by remote detection methods such as satellite SAR sensing (Engram et al., 2020). The quantification of CH₄ macroseepage to the atmosphere is challenging, because it involves irregular gas flowrates, which, taken individually, can range from few milliliters to tens of liters per minute (Walter Anthony et al., 2012), and are spatially and temporally unevenly distributed. When the gas flow rate is low, measurements are standardly done through quantifying the gas accumulation within a chamber, located at the surface of the ground (Rolston, 1986) or water (Etiope, 2015). This
- 55 approach, termed "closed chamber technique" in reference to the absence of a gas flowing through the chamber, is simple and easy to deploy and can be automated through a programmed venting device and a continuous gas analyzer, allowing repeated measurements over long-term periods without supervision (Davis et al., 2018; Martinsen et al., 2018). However, closed chambers have a fixed volume, in such manner that they are efficient for diffusive flux measurements combined with small ebullitive events (Tang et al., 2017), but are not applicable to large ebullitive fluxes. Indeed, the chamber capacity to
- 60 capture gas volumes is limited and any significant gas volume input, surpassing the chamber capacity, would escape from below the chamber, at the chamber/water interface.

An alternative method for the measurement of individual macroseeps is the use of submerged bubble traps. These consist of an inverted funnel, of variable design, placed underwater, in which the gas bubbles are collected during their ascent. This direct, simple and robust method is widely used for the determination of microbial CH₄ ebullition in aquatic ecosystems

65 (Walter et al., 2008; Wik et al., 2013; Delwiche and Hemond, 2017), and some automated designs have been suggested

(Varadharajan et al., 2010; Walter Anthony et al., 2010; Maher et al., 2019). Among these systems, very recently, Duc et al. (2020) have suggested a new design of an automated chamber, which allows for the autonomous measurement of diffusive and ebullitive CH_4 and CO_2 fluxes, based on an inverted funnel with a pressure-based automatic counting and release of the captured bubbles. However, bubbles traps are limited in size and capacity since maneuverability and avoidance of heavy

- 70 counterweights to compensate for the trap buoyancy are a concern (Bowen et al., 2008). Thus, these systems are well adapted for standard episodic bubble releases but are probably not the best option for macroseeps with large gas flowrates. A third method, commonly used, is an approximation of the flowrate to the atmosphere by examining the size and frequency of individual bubble trains, based on previous experiences and observed correlations (Etiope et al., 2004), or after field calibration of individual seeps with bubble traps (Walter Anthony et al., 2012). As described in the latter, this high
- 75 throughput method allowed for the quantification of thousands of individual seeps in northern lakes, through terrestrial and remote aerial observations. However, this method is probably subject to a large error, since for instance, a 10 % appreciation error in bubble diameter returns a 33 % error in bubble volume, and therefore in its CH₄ flux. In addition, bubble counting of fast rising trains is not an easy task.
- Although unreported so far for macroseepage in lakes, a fourth potential method is the use of underwater echo-sounders, which allow for bubble counting together with the determination of their sizes and rising speeds (Ostrovsky et al., 2008; DelSontro et al., 2011; McGinnis et al., 2011). However, to the best of our knowledge, this method has been applied to CH₄ seepage in marine environments (Jansson et al., 2019) but not to lake macroseepage. Despite their undeniable potential, these methods still present some uncertainty in quantifying gas emissions (Ostrovsky et al., 2008; DelSontro et al., 2015) and their applicability to intense trains of bubbles with a large size distribution is uncertain and would probably require intensive field
- 85 research before they could be validated. Moreover, hydroacoustic methods are limited to the ebullitive component of CH₄ emissions, thus a complementary method is required if diffusive flux needs to be quantified. A fifth method, based on floating chamber through which a CH₄-free carrier gas is continuously flowing, has been recently proposed (Gerardo-Nieto et al., 2019). That method, called Open Dynamic Chamber (ODC) allows for the combined and continuous monitoring of diffusive and ebullitive flux, but is limited to conditions where the ebullitive flow rate is relatively
- 90 small, compared to the carrier gas flowrate. These conditions impede the deployment of the ODC for large ebullitive fluxes like macroseepage.

There is therefore still a need for a field deployable method for flux determination of macroseepage in aquatic ecosystems, not only to update current seepage estimations, but also to monitor their expected progression. Preferably, the method should present the following attributes: (1) low-cost, small, light and robust, for easy field deployment in remote locations, (2) with

a high throughput capacity including large spatial coverage, and (3) able to measure CH_4 emissions in a large span of conditions, from low diffusive flux to large stochastic ebullitive events, with a single apparatus. The objective of this work was to develop a chamber design, the Mobile Open Dynamic (MOD) chamber, which fulfils these attributes, and to test it in a northern lake where large ebullition seeps have been detected. The accuracy of the MOD chamber was assessed through the parallel deployment of a 45 m² bubble trap.

2.1. MOD chamber

A rational approach to measure emissions from strong ebullitive seepage is to measure a sample of individual seeps and to multiply the measured emissions by the seep number (Walter Anthony et al., 2012). However, as we will show hereafter, precisely measuring the emission of individual seeps in aquatic environments is a difficult task. Based on field experience,

- 105 including testing several chamber designs and shapes, our trial/error approach gave birth to the Mobile Open Dynamic (MOD) chamber. The concept of the MOD chamber is based, similarly to the broadly used closed chamber, on the capture of the gas emitted from the lake into a cavity connected to a CH₄ detector. However, in the MOD chamber, a continuous air flow through the chamber is maintained and the CH₄ concentration is continuously monitored in the gas exiting the chamber. The concept of the open chamber; i.e. through which a carrier gas is flowing, was initially suggested by Edwards and Sollins
- 110 (1973) for the measurement of emission in soils and adapted later by Gerardo-Nieto et al. (2019) for aquatic ecosystems. However, three major differences distinguish the MOD chamber concept from these previous works; (i) atmospheric air is used as carrier gas, as opposed to CH_4 -free nitrogen gas, avoiding the requirement of heavy compressed gas cylinders, (ii) the concept and mass balance of the MOD chamber allows quantification of CH_4 emissions with a significant volumetric flowrate, and (iii) the chamber is designed to be mobile; i.e., in motion during continuous transects measurement. We
- 115 engineered chamber mobility for several important reasons. First, we will show that positioning a measurement apparatus exactly over a macroseep is very challenging in the absence of a stable ice platform, not only because any floating device is subject to a constant and unavoidable movement caused by wind and waves, but also because the seep itself causes water convection at the lake surface that pushes the trap off of the bubbling hotspot. In motion, a well-designed chamber can cross macroseeps without being diverged. The second reason is that the measurement of macroseeps involves high ebullition
- 120 entering the chamber, while a mobile chamber passing over a macroseep accumulates a limited quantity of gas during the short period of time, and as we will show hereafter, these conditions avoids the requirement of a gas flow rate measurement, which is technically very challenging with stochastic and discontinuous ebullition. The third reason is that strong ebullition in lakes has been repeatedly reported to occur in fixed locations (Walter et al., 2006; Walter Anthony et al., 2012) (e.g. point-source seeps; illustrated by Fig. S1), each one with a specific relative overall magnitude. Thus, an approach based on
- 125 measuring individual seeps and counting, is a relatively easy task but requires an arbitrary classification, while transecting at constant speed gives the same specific weight to all measurements done along that transect, including low-flux and hotspot-flux seeps of variable magnitude. Despite these potential benefits, we acknowledge that the chamber motion has undoubtedly some effect on the gas/liquid boundary layer at the surface of the lake (Schubert et al., 2012; Lorke et al., 2015), which in its turn may modify substantially the diffusive flux captured by the chamber, compared to a steady interface. This effect was

130 quantified during field testing.

The conceptual sketch of the MOD chamber is presented in Fig. 1; specific dimensions are presented in Fig. S2 and a superior and inferior view of the chamber hull is presented in Fig. S3. This aluminum chamber consists of two half-tubes

separated by a short distance, serving as a double hull, oriented perpendicular to the main longitudinal axis; i.e., motion axis. An aluminum sheet laterally covers these half-tubes as well as the top of the space between them, thus defining a chamber

- 135 volume. The bottom of this headspace is open to collect gas emitted from the lake. The use of two half tubes in contact with water avoids straight angles along the motion axis. Together with a limited draft, this design minimizes mixing of the water surface while moving at low speed. Therefore, it reduces the effects of motion on the air/water boundary layer. In addition, the lateral aluminum foils fulfill the function of a double keel, reducing lateral movement while crossing hotspots. A fixed flowrate of the chamber content is extracted to a CH₄ detector. A purging vent allows for pressure equilibration and an
- 140 electric fan located inside the chamber ensures homogeneity of the gas phase.

2.2. Mass balance of the MOD chamber

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Whatever the type of emission; i.e., diffusive or ebullitive, the CH_4 mass balance of the MOD chamber can be described by Eq. (1), which considers a CH_4 input caused by lake emissions (first term), a CH_4 output caused by the CH_4 analyzer extraction flowrate (second term), and an input or output of gas through the purge (third term), used to equilibrate pressure between the chamber and the atmosphere (See Fig. 2 for details)

$$\frac{dC_C}{dt} = F \cdot \frac{A_C}{V_C} - \frac{Q_D}{V_C} \cdot C_C + \frac{Q_P}{V_C} \cdot C_P \tag{1}$$

where C_C is the CH₄ concentration in the headspace of the chamber (g m⁻³), which is considered completely mixed, *F* is the CH₄ flux emitted by the lake, diffusive and/or ebullitive (g m⁻² s⁻¹), A_C is the area of the chamber in contact with the water surface (m²), V_C is the volume of the chamber (m³), Q_D is the air flowrate extracted from the chamber to the detector (m³ s⁻¹);

150 Q_P and C_P are respectively the gas flowrate (m³ s⁻¹; positive for incoming flow) and the CH₄ concentration (g m⁻³), entering or exiting the chamber through the purge.

The pressure equilibration guaranteed by the purge, results in a constant chamber volume and dictates that its flowrate; Q_P , depends on the ebullitive gas flowrate (Q_B) and the gas flowrate extracted by the detector (Q_D), which is described by Eq. (2):

(2)

$$155 \quad Q_P = Q_D - Q_B$$

Thus, if the Q_B captured by the chamber is greater that the Q_D , the resulting Q_P is negative; i.e., the purge allows headspace gas to flow out of the chamber, and C_P is equal to C_C . On the contrary, if Q_B is smaller than Q_D , the resulting Q_P is positive; i.e., the purge allows atmospheric air to flow into the chamber, and C_P is equal to the atmospheric CH₄ concentration; C_{ATM} . By substituting Q_P in Eq. (1), we obtain a general mass balance equation:

$$160 \quad \frac{dC_C}{dt} = F \cdot \frac{A_C}{V_C} - \frac{Q_D}{V_C} \cdot C_C + \frac{Q_D - Q_B}{V_C} \cdot C_P \tag{3}$$

Considering that the chamber would be constantly in motion, passing persistently over low-flux and hotspot-flux ebullition seeps, the mean ebullitive flowrate captured would be reduced, and the condition $Q_D > Q_B$ may occur. Under this scenario, Q_P would be positive (Eq. (2); gas flowing-in the chamber through the purge), C_P is replaced by C_{ATM} , and Eq. (3) becomes:

$$\frac{dC_C}{dt} = F \cdot \frac{A_C}{V_C} - \frac{Q_D}{V_C} \cdot C_C + \frac{Q_D - Q_B}{V_C} \cdot C_{ATM}$$
(4)

165 During field deployment of the chamber, we observed that CH₄ accumulated rapidly into the chamber, reaching a concentration several order of magnitude above atmospheric air ($C_C > C_{ATM}$). In addition, ($Q_D - Q_B$) is inevitably lower that Q_D , in such manner that the third term of Eq. (4) is negligible compared to the second term. Thus, after simplification, and solving Eq. (4) for *F*, we obtain:

$$F = \left(\frac{dC_C}{dt} + \frac{Q_D}{V_C} \cdot C_C\right) \cdot \frac{V_C}{A_C}$$
(5)

170 It is important to note that in Eq. (5) the only flowrate required is Q_D , which is a design parameter; i.e., flowrate of the detector's internal pump, which can be easily measured and calibrated. Thus, through motion of the chamber, the conditions where $Q_B < Q_D$ is beneficial for data interpretation as it avoids the requirement of Q_B determination. The mean flux (\overline{F}) emitted by the lake over a time lapse (Δt) is given by Eq. (6), where $\overline{C_C}$ is the mean C_C measured, and which can be easily numerically solved and eliminates the impact of the measurement noise.

175
$$\overline{F} = \left(\frac{\Delta C_C}{\Delta t} + \frac{Q_D}{V_C} \cdot \overline{C_C}\right) \cdot \frac{V_C}{A_C}$$
(6)

2.3. Chamber design

Figure S2 shows the dimensions of the MOD chamber prototype and Fig. 3 shows the prototype while being operated. The 8.56 kg chamber was formed and welded from 3/32" (2.3 mm) thick aluminum sheet. Its total length was 95 cm long. The draft of the chamber was limited to 6 cm, and because of the cylindrical hull, the buoyancy (kg) was a power function of the

- 180 draft (cm; buoyancy = 0.65 · Draft^{1.44}), ensuring better vertical stability. It is worth noting that the pressure inside the chamber was in equilibrium with the atmospheric chamber, through the 1" purge tubing (see below), thus ensuring a constant draft and chamber volume and area. The open contact area with water was 0.109 m² and the volume of the chamber was 10.8 L. The chamber content was homogenized with a 2" battery operated fan (explosion proof), located inside the chamber volume. The chamber was connected to a CH₄ detector; we used either an EX-TEC (HS 680, Sewerin, Germany), or an ultraportable
- 185 greenhouse gas analyzer (UGGA, Los Gatos Research, CA). Both detectors had a data acquisition frequency of 1 Hz. The EX-TEC featured a gas sampling rate (Q_D ; internal pump) of 1.4 L min⁻¹, a CH₄ lower detection limit (LDL) of 1 ppmv and a measurement range of 0–100 % v/v. The UGGA, equipped with the extended range option, included a gas sampling rate of 1.1 L min⁻¹ (Q_D), and a CH₄ concentration measurement range of 0–10 % v/v with a CH₄ LDL of 0.01 ppmv.
- In addition, the chamber was also equipped with a purge, which consisted of a 1" internal diameter steel tubing, a water trap and an airflow sensor with high sensitivity at low flow rates (AWM720P1, Honeywell, Mexico). This flow sensor's measurement range was 0 to 200 L min⁻¹ for both positive and negative flows, corresponding to a pressure drop of 0 to 2.74 mbar. To reduce wind effects on the airflow sensor, the output of the sensor was covered with open-cell polyurethane foam. In order to reduce weight and thus the draft of the chamber, the MOD chamber was attached with a loose line and a stick, at

the front of a small inflatable Alpacka Packraft, where the operator was, and in which the detectors and the batteries were placed.

2.4. Site description

The MOD chamber was tested at Esieh Lake (informal name), a 6.4 ha lake, located 40 km north of Kotzebue in northwestern Alaska (67.249, -162.735) on August 21–26, 2018. At the time of the measurement campaign, Esieh Lake was characterized by sections with constant and intense ebullition (i.e. macroseepage), surrounded by large areas where no ebullition was observed. In addition, some calibration experiments were done at "Lago de Guadalupe" (LG; 19.633, -99.260), a 450 ha subtropical dendritic reservoir located at 2300 m above mean sea level, 25 km north of the Mexico City limits. This lake was characterized by a relatively small western section with moderate ebullition and an eastern section, in which no ebullition was observed.

2.5. Flux measurements and data interpretation

- A section of Esieh Lake with intense ebullition was used to test the MOD chamber. The procedure was as follows; (1) the chamber was lifted out of the water and ventilated for one minute, (2) then the chamber was gently positioned on the surface of the water, (3) the chamber was immediately put in motion, at a speed of approximately 0.30 m s⁻¹, while (4) the detector was continuously recording CH₄ concentration, and a GPS (GPSmap 76 CSX, Garmin, USA) was recording the monitoring track. Measurement and motion were maintained, until a significant CH₄ concentration increase was observed in the
- 210 chamber, usually reaching the volume percent range, or when the zone with high ebullition was traversed. This procedure was repeated for a total of 15 transects during the field campaign. In the section of the lake where no ebullition was observed, the MOD chamber was also tested for diffusive flux measurements. With that purpose, the same strategy was used, except that the chamber was maintained stationary, the purge was closed and the CH₄ detector was connected in a loop. CH₄ measurements were started about 30 s after positioning the chamber on the lake surface, to allow for equilibration, and
- 215 measurement was sustained for 3 minutes each. During the field campaign, a total of eight triplicate diffusive flux measurements were done.

As it is shown in the Results and Discussion section, during transects or stationary measurements, a continuous increase of the CH₄ concentration read by the detector (C_D) was observed, as expected, with some abrupt rises when bubbles entered the chamber. The data interpretation (described in detail in section S1) included the conversion of C_D data from ppmv (as read

- by the detectors) to mass units (g m⁻³), using the ideal gas law. Then, the determination of CH₄ concentration in the chamber (C_C) was determined, from C_D , taking into account the response time of the system, determined in the field. Indeed, even if it can be assumed that a bubble entering the chamber is immediately mixed within the chamber, the detectors have an inherent response time (θ) . This effect causes a certain delay and a buffer time, between the actual concentration read by the detector C_D and C_C . To take this delay into account a standard mixing model was used during the data treatment process, which is
- described in detail in the supporting information section (Section S1). From C_C data, flux time series were established, after

data smoothening (Section S1). In addition to *F* determinations, the step increases of C_C were exploited to determine the CH₄ content of the bubbles (M_B), according to a simple procedure, as well as the volume of the bubbles (V_B) and their equivalent spherical diameter (d_B), according to eqs S5 and S6, after determining the CH₄ bubble percentage of 83.4 % v/v (see results section).

- For mapping purposes, to avoid interpolating large dataset (one *F* and one location for each second of measurement), each transect was segmented into 3 to 5 subdivisions, typically 10 m long. The mean flux for each segment was determined according to Eq. (6), and the central coordinates of the segment was considered for mapping. A map of CH₄ emissions was established from *F* data interpolation using Surfer 11.0 software (Golden Software, USA). The selection of the best interpolation method among Kriging, Minimum Curvature, Inverse Distance to a Power, Radial Basis Function, and Local Polynomial was based on two criteria: the mean absolute error and the mean bias error (Wilmott and Matsuura, 2006).
- Fluxes determined at Esieh Lake with the MOD chamber were compared to a direct bubble trap measurement in an area of the lake that was approximately 4 m deep. The bubble trap consisted of an octagonal pyramid, with an open base area of 45 m² and approximate height of 2 m. The walls of the pyramidal were made of plastic sheeting and fixed on a PVC tubular structure (Figures 4 and S4). At each corner of the structure, an anchor and a float were fixed in such a manner that the
- funnel was steadily positioned under water at about 1 m above sediments. At the center of the funnel, an additional float was fixed to keep the pyramid taut. At the top of the bubble trap, a specially manufactured union connected the inner volume of the pyramid to a straight 2" pipe, of 3 m length that was kept in vertical position. A Pitot tube with a high frequency 0–500 Pa differential pressure sensor was used to measure the gas speed, and therefore the gas flow rate collected by the bubble trap. The CH₄ flow was formed by discrete bubbles, and as such, the signal had a high degree of both high-frequency and
- 245 low-frequency variability. Flow data was recorded for 2 second each minute, to filter out high-frequency signals. Multiple minutes worth of samples were averaged in order to determine the actual flow rate. The bubble trap in operation was calibrated by comparing the measured flow rate and the time required to fill a 155 L plastic bag. This bubble trap was deployed on August 27, 2018; i.e. just after MOD chamber deployment.
- In addition to field testing at Esieh Lake, the impact of motion on diffusive flux measurements was quantified using the same chamber in a section of "Lago de Guadalupe" where no ebullition was observed. In this case, the MOD chamber was operated with a continuous flow of CH_4 -free nitrogen, exactly as the ODC method (Gerardo-Nieto et al., 2019), from a small guiding boat powered by an electrical fishing engine with speed control. The chamber was kept stationary for several minutes during which *F* was measured constantly; then, the chamber was put in motion at a speed of approximately 0.56 m s⁻
- ¹ (2 km h⁻¹), intentionally above the maximum speed reached during the transects at Esieh Lake. The chamber was kept in motion until relatively stable readings were obtained. It is worth noting that this method was applied in "Lago de Guadalupe" instead of Esieh lake because the ODC method used (with the MOD chamber) required and electric powered boat, compressed gas and gas flow control, unavailable at the remote location of Esieh Lake.

3 Results and discussion

During the field campaign, the MOD chamber was first tested in a still position in a region of Esieh Lake where high

- 260 ebullition was observed. During this first test, keeping the chamber exactly over an ebullition hotspot was identified as a difficult task, due to boat motion caused by wind and waves, but also because large bubble seeps generated strong radial water movement at the surface, pushing the chamber outward away from the center of hotspot seeps. In addition, even when a gas burst was captured by the chamber, the airflow sensor did not produce a clear signal among the large noise. We linked that noise to stochastic ebullition and strong agitation caused by the seep, causing pressure and flowrates oscillations. In 265 contrast, we observed that, when in motion, the chamber was able to cross hotspots without being diverted, probably thanks to the keels and the kinetic energy of the chamber in straight motion. Due to the difficulties of maintaining stationary positions and accurately measuring Q_B , the measurement of high ebullition at stationary location was quickly abandoned in
- During the field campaign we measured CH₄ emissions in a selected 3500 m² macroseepage area (Movie S1), where strong ebullition was observed. In that section, 15 transects for a total of 72 flux measurements were done. We also made eight stationary diffusive flux measurements next to the macroseepage area where ebullition was not observed. Paddling under variable wind velocities and directions made it difficult to maintain a constant boat speed along the transects. Overall, during the 15 transects, the mean transect speed, determined from the length and the duration of the transect; i.e. not relying on imprecise GPS speed indicators, ranged from 0.19 to 0.50 m s⁻¹, with a mean of 0.30 ± 0.09 (mean \pm one standard deviation

favor of ebullition flux measurements in motion, which does not require flowrate measurement.

of the mean). It should be highlighted that the speed during transect has no effect on the method, except the effect that motion has on diffusive fluxes, which will be discussed later. The distance covered by each transect was 42 ± 14 m. A typical example of the results obtained during a transect is shown in Fig. 5A (additional example shown in Fig. S5), during which four sharp C_D increases were detected. A total of 10 of these abrupt C_D increases were used to fit Eq. (S2) and to determine θ , which was relatively constant at 11.35 ± 3.13 s (results not shown) with a coefficient of determination (R²) of 0.001 ± 0.007

 $280 \quad 0.991 \pm 0.007.$

From the same data set, the instantaneous flux was determined using Eq. (5) and is presented in Fig. 5B. As shown, despite double data smoothening, a significant noise was still observed. The exact contributions of the lake CH₄ flux and the MOD chamber method to that noise is uncertain, although differences in noise were observed within a single transect or among different transects, which indicates that part of the noise was caused by the lake bubbling dynamics. Despite noise, the mean

F measured from Eq. (5) during transects was equal to those estimated from Eq. (6) and had therefore no impact on overall *F* determinations. The mean *F* determined from the transects in the selected ebullition zone of the lake was highly variable, as shown on Fig. S6.A, and ranged from 3.4×10^1 to 2.8×10^4 g CH₄ m⁻² d⁻¹; i.e. over 3 orders of magnitude, with a mean and standard deviation of the mean of 2518 ± 5379 g CH₄ m⁻² d⁻¹.

To confirm the potential of the MOD chamber to also measure diffusive fluxes we conducted stationary measurements adjacent to the macroseepage site, but in an area where no clear ebullition was observed. On average, the mean diffusive flux from the water adjacent to the macroseepage area was 27.5 \pm 21.6 g m⁻² d⁻¹ (data not shown). This is about 3 orders of magnitude above mean diffusive fluxes from lakes north of 66° N (Wik et al., 2013; Bastviken et al., 2011), and suggests that the intense ebullition observed promotes CH₄ transfer to the water column and triggers diffusive fluxes.

- We created a CH₄ emission map by interpolating data collected from these transects and stationary measurements (Fig. 6). 295 Mean emission from the interpolated data was of 1226 g CH₄ m⁻² d⁻¹, which corresponds to a total daily emission of 4.2 tons of CH₄ over the entire 3500 m² lake section that was selected. Five hours of continuous measurement of the gas collected by the bubble trap on August 27 showed a highly variable flowrate of 31 ± 34 L min⁻¹. The CH₄ content of the collected bubble gas was determined by gas chromatography (83.4 % v/v; J. Chanton's laboratory, Florida State University), which allowed to determine a mean CH₄ emission of 575 ± 618 g CH₄ m⁻² d⁻¹ (Fig. S7). In order to better compare emissions determined by
- 300 the MOD chamber and the bubble trap, the position of the latter was localized on the CH₄ emission map with a 4 m error range, which reflects potential coordinates error between MOD chamber and bubble trap deployments, and is represented by the red discontinuous circle in Fig. 6. When considering any position of the bubble trap within that circle, the mean mapbased emission; i.e. determined from interpolated MOD chamber measurements, was 542 ± 522 g CH₄ m⁻² d⁻¹, thus showing no significant difference between the MOD and bubble-trap methods. The mean emission in the selected section of Esieh
- 305 Lake is within reported range for seepage (Etiope, 2015), 4 orders of magnitude higher than mean emissions from lakes northward of 66°N (Bastviken et al., 2011; Wik et al., 2013), and 2 orders of magnitude above the mean emission reported for wetlands (Kayranli et al., 2010). The total daily emission of the selected area, estimated to 4.2 tons of CH₄, is of the same magnitude as emissions reported for macroseepage globally (Etiope, 2015).
- From the emission determined in the selected section of Esieh Lake, considering 83.4 % CH₄ content in bubbles, the gas 310 emission flowrate observed during transect measurements ranged from 5.8×10^1 to 4.9×10^4 L m⁻² d⁻¹ or 0.04-34 L m⁻² min⁻¹. Similarly, from the abrupt C_C increases, the CH₄ content of the bubbles (M_B) and their size (d_B) was determined, which is a potential additional benefit of the MOD chamber. These parameters are indeed the most important parameters that affect ebullitive CH₄ transport through the water column and to the atmosphere (DelSontro et al., 2015; Greene et al., 2014). Overall, M_B ranged from 1.23 to 781 mg CH₄ with a mean of 81 ± 144 mg CH₄. The corresponding bubble diameter ranged
- 315 16–138 mm, which is within standard bubble diameter considered in seep flux estimations (Etiope et al., 2004) but does not match visual observations since numerous small bubbles were observed at Esieh lake. This suggest that the MOD chamber method does not detect and quantify small bubbles, although these small bubbles are included in *F* measurements. Small bubbles might be the reason why high flux noise was observed during transect measurements (Fig. 5B).
- The ebullitive flowrate reaching the MOD chamber (Q_B) was determined to 0.33 ± 0.71 L min⁻¹, thus validating the condition 320 $Q_B < Q_D$ that was considered during this work. However, it is worth noting that, in five occasions over a total of 74 flux measurements, Q_B was temporarily exceeding Q_D , showing that the MOD chamber, as applied in Esieh Lake, was reaching its overall maximum flux measurement capacity. Considering the condition $Q_B = Q_D$ as the frontier condition, the prototype configuration used allowed for the measurement of a maximum steady flux of 8.4×10^3 to 1.08×10^4 g CH₄ m⁻² d⁻¹ (equivalent to 10.1-13.0 L m⁻² min⁻¹ of 83.4 % CH₄ bubbles), with the UGGA and the EX-TEC detector, respectively.

- 325 Nonetheless, it should be kept in mind that this upper limit of the MOD design is proper to the chamber design tested at Esieh Lake. Indeed, an additional extraction pump, working at a precise flowrate, could be added to the configuration of the MOD chamber, without any modification of the mass balance equations (if C_C is kept far above C_{ATM}). That additional pump would allow increasing Q_D above the flowrate extracted by the detector and make the MOD chamber applicable to practically unlimited flux intensity. However, it is of crucial importance for Q_D to be well known, to avoid error in the mass
- balance. Thus, the additional pump used should ensure constant flowrate and be precisely calibrated. From our results, these arguments, and the previously established difficulty to measure macroseepage hotspots at fixed locations, we conclude that the MOD chamber working at $Q_B < Q_D$, is a resourceful option for seeps measurements. An important point left to discuss is the effect of chamber motion on the diffusive component of CH₄ flux. Any water
- movement affects the gas/liquid boundary layer, which is of crucial importance in mass transfer (Schubert et al., 2012; Lorke
 et al., 2015). By using an expressly designed chamber, we tried to reduce this impact, but still, the diffusive CH₄ flux during rowing transects might have been overestimated at Esieh Lake. To test that impact, the MOD chamber was deployed in a region of Lago de Guadalupe where no ebullition was observed. We compared the flux measured continuously in a stationary, drifting position without rowing and then in motion at approximately 0.56 m s⁻¹, which is on purpose above the maximum speed during transects in Esieh Lake. The results, presented in Fig. S8, show measured fluxes in a relative scale.
- We observed that F during motion was 2.1 to 3.4 times higher compared to F under stationary conditions and the mean increase factor was 2.8, confirming that the chamber motion decreases the boundary layer thickness and artificially increases the diffusive flux. It should be noted, that during these tests, the speed indicator used was our GPS, which is highly unprecise at such a low speed, and might explain at least part of the important noise observed during motion, as well as differences between replicates.
- To quantify that impact on *F* measured at Esieh Lake, we isolated diffusive fluxes events, observed during transects. Indeed, transects and *F* determinations were started in regions of the lake where little or no ebullition was observed, steering toward regions with high ebullition. Thus, in many cases, the initial measurements were done while moving but with diffusive flux only. These diffusive fluxes ranged 4.8–230 g m⁻² d⁻¹, with a mean of 64 ± 57 g m⁻² d⁻¹, (*n* = 14; Fig. S6.B). This mean diffusive flux represented 2.56 % of the mean total flux measured during transects, thus, if this diffusive flux was overestimated 2.8 times (as shown on Fig. S8), the error committed would have been an overestimation of 1.65 % of the total

F.

The new concept of a dynamic chamber moving at the surface of a lake showed several benefits for the measurement of emissions from lakes with intense CH_4 ebullition seeps. The main features that makes the MOD chamber of interest is that while moving, each point along a transect is sampled with the same statistical relative weight. It dispenses with the complex

355 chamber positioning over hotspots, does not require the measurement of the gas flowrate emitted by the lake, and does not involve an arbitrary classification of individual seeps. Unlike the large bubble trap which was limited to a fixed position and required four people for fieldwork, the MOD was lightweight and easily operated by one person. We demonstrated experimentally that this method allows for the measurement of emissions of up to 1.08×10^4 g CH₄ m⁻² d⁻¹. However, this theoretical border is not a fixed limit, since the addition of an extractor with a higher flowrate would allow, in theory,

- 360 measurement of higher emission magnitude. We also confirmed that the same chamber could be used for low diffusive fluxes, which is not surprising as the MOD chamber is similar to static chambers when operated as a closed loop under static position. Thus, the MOD chamber is versatile by covering the entire magnitude range of CH_4 emissions currently identified in aquatic systems. A comparison to other methods is difficult, because to the best of our knowledge, none of them have been used to measure macroseeps such as those found at Esieh Lake. However, among those that could be theoretically used
- with the same purpose (Table S2), the MOD chamber is the single method allowing measurements under motion or static position and covering the entire range of aquatic ecosystem emissions, from low diffusive flux to large ebullition seeps, with a single apparatus. Regarding costs, the MOD chamber is moderately expensive. It requires a CH₄ analyzer, which is the costliest component, ranging from about 10,000\$ (cost of the Ex-Tec) to 50,000 US\$ (cost of the UGGA). However, any CH₄ detector with moderate sensitivity could serve, and a low-cost detector as the model used by Duc et al. (2020) could be
- 370 convenient.

Despite the promising results obtained, we acknowledge that the concept tested would greatly benefit from further research. First, we observed that chamber motion affects diffusive flux measurements, at least to a minor extent, in such manner that the development of a precise speed controlling device as well as a more systematic evaluation of speed impact would be of great interest. Second, the MOD chamber design was conceptually developed from a trial/error approach, which included

- 375 testing several chamber designs and shapes. A more systematic direct engineering approach, for instance, including computational fluid dynamics studies, might lead to an improved design. Hence, the design suggested here is already operational and field validated for its use on lakes with CH_4 ebullition seeps during ice free conditions. Its potential use under other configurations might be foreseen. For example, the use of the same concept on bubble-induced open holes in lake ice might be considered. In this case, the chamber should be used in stationary position, which has been shown difficult
- 380 in the present work, but the presence of ice around the seeps might greatly facilitate firm positioning, thus avoiding the problem encountered at Esieh Lake

4 Conclusion

The method suggested here is operational and field validated for its use on lakes with CH₄ emissions ranging the entire magnitude of CH₄ emissions currently identified, from those standardly observed in lakes to intense macroseeps, with a single apparatus of moderate cost. The MOD chamber is a promising method for the determination of seepage in aquatic environments, not only with the objective to update current seepage estimations, but also to monitor their expected increase as permafrost thaws and large gas seeps potentially become more abundant in the future.

Data availability. The data associated with this work are stored at; Thalasso, Frederic (2020), "MOD chamber HESS data", 390 Mendeley Data, V1, doi: 10.17632/kpbc6mhwjt.1 *Supplement*. The Supporting Information includes 8 pages, 8 Figures, 1 movie, 2 Tables and 7 equations, available online at: Mendeley Data, V1, doi: 10.17632/2k4ztzsmkd.1

395 Author contribution. FT and KWA conceived the study. FT wrote the paper. FT and RGV analyzed the MOD data. OI, EC, and LB were responsible for the large bubble trap analysis. All authors except RGV contributed to field work. All authors have given approval to the final version of the manuscript.

Competing interests. The authors declare that they have no conflict of interest.

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Acknowledgments. The authors thank Francisco Silva-Olmedo, David Flores-Rojas, and Andrés Rodríguez Castellanos for their technical assistance. Janelle Sharp, Oscar Gerardo-Nieto, and Yameli Alfano-Ojeda assisted with field work. The NANA Regional Corporation granted permission and logistical support for field work at Esieh Lake. This work was supported by the "Consejo Nacional de Ciencia y Tecnología" (Conacyt, project 255704) and NASA ABoVE NNN12AA01C.

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Figure captions

550 Figure 1: Conceptual sketch of the mobile open dynamic (MOD) chamber, shown at the surface of the lake, passing over an intense seep (A); Cross section of the chamber cavity (B). Darker and lighter blue colors indicate three aluminum sheets welded together.

Figure 2: Mass balance of the MOD chamber (see text for details).

555 Figure 3: Prototype being operated on Esieh Lake (Credit: K. Walter Anthony).

Figure 4: Bubble trap shown during installation before it was submerged (A) and during operation (B); the inflatable boat contained the measurement device at the center of the submerged bubble trap (Credit: O. Irzak).

560 Figure 5: Typical example of; (A) C_D (grey solid line) and C_C (black solid line) measured during a transect, and (B) instantaneous flux computed from these concentrations. Blue arrows show when large bubbles were captured by the chamber and red marker shows an example of ΔC_C used to determine the CH₄ content of the bubbles (see Section S1). Please note the logarithmic scales.

Figure 6: Map of CH₄ emissions in a region of Esieh Lake with large gas seeps; black crosses (+) indicate central location of transects measurements. This map scale is metric; i.e. same distance scale in both axes. Please note the logarithmic color scale. Red octagon indicates the location of the bubble trap, while the dotted red circle represents potential coordinates error between MOD chamber and bubble trap deployments; i.e. ± 4 m, see text for details).

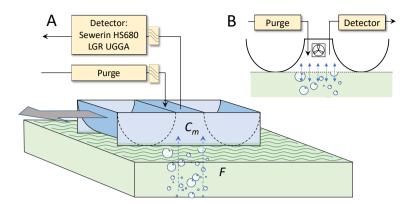


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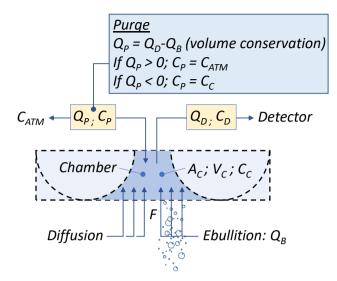


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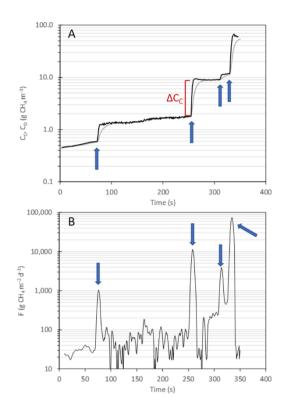


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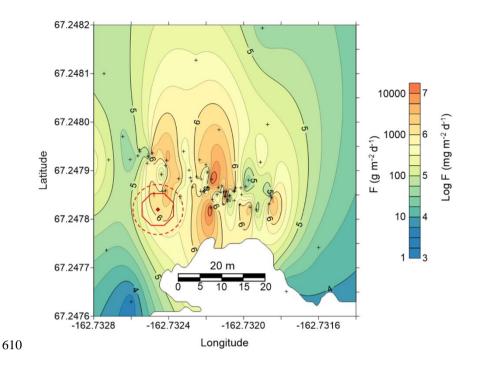


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Marked supplementary information Mobile open dynamic chamber measurement of methane macroseeps in lakes

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Supporting Information:

Number of pages: 8 Number of Figures: 8 Number of movies: 1 Number of Tables: 2 Equations from S1 to S7

Table S1: Notations.					
Notation	Description	Units			
А	Area	m^2			
С	Gas concentration	g m ⁻³			
d	Diameter	m			
F	Gas flux	$g m^{-2} s^{-1}$			
g	Standard gravity	m s ⁻²			
Μ	Mass	g			
Р	Pressure	atm			
Q	Gas flowrate	$m^3 s^{-1}$			
R	Universal gas constant	L atm mol ⁻¹ K ⁻¹			
Т	Temperature	Κ			
V	Gas volume	m ³			
% _{CH4}	Volume percentage of CH ₄ in bubbles	%			
θ	Response time	S			
ρ	Volumetric density	kg m ⁻³			
Subscripts					
Р	Purge				
В	Bubble or ebullition				
D	Detector				
С	Chamber				
ATM	Atmospheric				
t	Time				

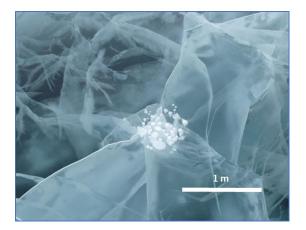


Figure S1. Methane bubbles trapped in the ice of an arctic lake, illustrating that ebullition occurs repeatedly in specific locations (Credit: A. Sepulveda-Jauregui, F. Thalasso).

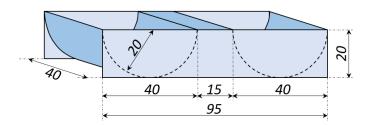


Figure S2. Dimension of the prototype built and used in the present work. Darker and lighter blue colors indicate three independent aluminum foils welded together. Dimensions are in cm.

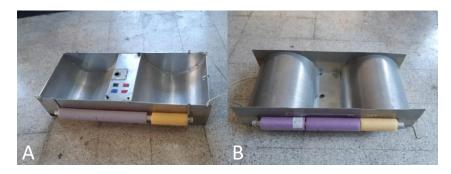


Figure S3. Superior (A) and inferior (B) view of the chamber hull with lateral floats added for improved stability.



Movie S1. Methane seeps; general and closeup views. Available at: Thalasso, Frederic (2020), "Esieh lake seepage HESS", Mendeley Data, V1, doi: 10.17632/fnr3mkxmk9.1

S1. Response time and data interpretation

The concentration read by the detector has a certain delay, due to the gas residence time from the chamber to the detector. However, if the detector is close to the chamber and the tubing of a reduced diameter, this time is very short; i.e., from 1.6 to 2.0 s in our case. However, even if it can be assumed that a bubble entering the chamber is immediately mixed within the chamber, the detectors have an inherent response time. This effect causes a certain delay and a buffer time, between the actual concentration read by the detector (C_D) and C_C . To take this delay into account a standard mixing model can be used (Eq. S12), where θ is the response time of the system

$$C_C = \left(\frac{dC_D}{dt} \cdot \theta\right) + C_D \tag{S1}$$

In Eq. (S1), θ was determined from experimental data, using several step C_D increases observed in the field. The adjustment was done through excel, minimizing the Root Mean Square Error (RMSE) between experimental C_D data and Eq. (S2), where $C_{D,\theta}$ is the initial reading of the detector (at time 0), and C_C is the actual concentration in the chamber.

$$C_D = C_{D,0} + \left[(1 - \exp(-t/\theta)) * (C_C - C_{D,0}) \right]$$
(S2)

After C_C was determined, Eq. (5) was used to determine instantaneous F along the transects. Alternatively, Eq. (6) was used to determined mean flux over a transect section. In the case of instantaneous F, during transects, and despite the relatively high signal to noise ratio of detectors used; i.e., ratio of the mean to the standard deviation, F was subject to a significant noise, and a first data smoothening of C_C was necessary, followed by a second smoothening of dC_C/dt (Eq. S7). In both cases we opted for a pondered smoothening described by Eq. S3, where X' is the smoothened variable X, in this case C_C or dC_C/dt .

$$X'_{t} = 0.1 \cdot X_{t-2} + 0.2 \cdot X_{t-1} + 0.4 \cdot X_{t} + 0.2 \cdot X_{t+1} + 0.1 \cdot X_{t+2}$$
(S3)

As it will be shown in the Results and Discussion section, peak fluxes were detected, which corresponded to step increases of C_C (ΔC_C), caused by bubbles reaching the chamber. These abrupt increases offer a unique opportunity to quantify the CH₄ mass content of the bubbles (M_B). It should be noticed that since these step increases were observed in a few seconds, the amount of CH₄ lost through detector extraction or entering the chamber can be neglected over that short time, as far a as single and clear increase was observed. Thus, M_B was determined during the field experiment according to Eq. (S4).

$$M_B = \Delta C_C \cdot V_C \tag{S4}$$

From M_B , the volume of the bubbles (V_B) and their equivalent spherical diameter (d_B) at atmospheric pressure were determined, assuming that the CH₄ content in the bubbles ($%_{CH4}$) is known, according to Eq. (S5) and (S6), respectively.

$$V_B = \frac{M_B}{16} \cdot \frac{R \cdot T}{P} \cdot \frac{1}{\mathscr{N}_{CH4}}$$
(S5)

$$d_B = 2 \cdot \sqrt[3]{\frac{3 \cdot V_B}{4 \cdot \pi}} \tag{S6}$$

where 16 is the molecular weight of CH₄ (g), *R* is the universal gas constant (L atm mol⁻¹ K⁻¹), *T* is the temperature (K) and *P* is the atmospheric pressure (atm).

Since bubble volume and diameters are important for mass transfer determination during their migration to the lake surface, the actual bubble volume (V'_B) at a given depth (D) within the water column is given by Eq. (S7).

$$V'_{B} = V_{B} \cdot \frac{P}{\frac{(\rho \cdot g \cdot D)}{101,325} + P}$$
(S7)

where ρ is the water volumetric mass density (kg m⁻³), g is the standard gravity (m s⁻²), and 101,325 is the conversion factor from Pa to atm.

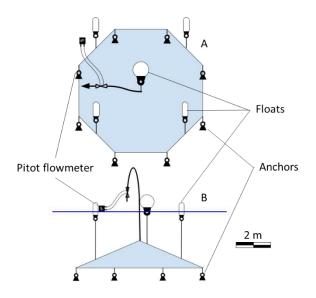


Figure S4. Conceptual sketch of the bubble trap used at Esieh Lake; (A) top view, (B) front view.

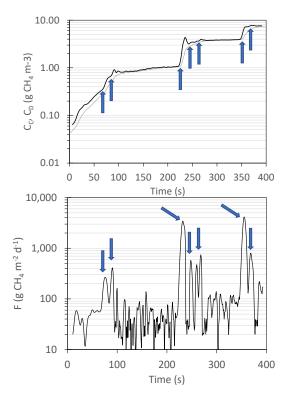


Figure S5. Additional example of; (A) C_D (grey solid line) and C_C (black solid line) measured during a transect, and (B) instantaneous flux computed from these concentrations. Blue arrows show when large bubbles were captured by the chamber. Please note the logarithmic scales.

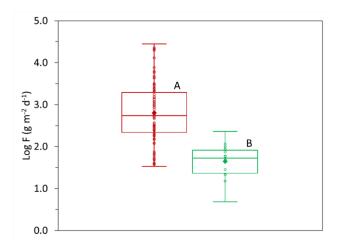


Figure S6. Box and whiskers showing statistical distribution of fluxes measured with the MOD chamber (A, n = 74) and the diffusive component of these fluxes (B, n = 14; see text for details). Boxes show interquartile range and median, whiskers represent minimum and maximum, open circles show raw data and filled diamonds represent arithmetic mean.

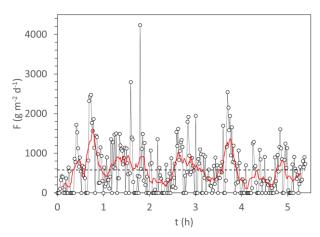


Figure S7. Flux measured by the bubble trap. Each discrete value is the average of 1 minute of continuous measurement. Horizontal discontinuous line shows the mean flux while red continuous line shows 10 minutes moving average of F data.

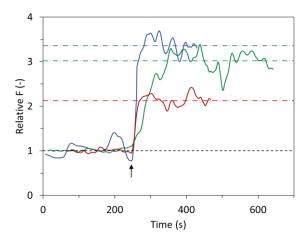


Figure S8: Relative fluxes observed with the MOD chamber, under stationary position (left of the arrows) and under motion. Data are presented in relative units, one being the flux observed in stationary position. Horizontal dot-dashed lines represent the mean fluxes during motion.

Table 32 . Comparison of four methods with a potential to be used in take seepage.					
	Bubble trap	Duc et al. (2020)	Hydroacoustic	MOD Chamber	
Large seeps	Yes	Potentially Yes	Potentially Yes	Yes	
Diffusive flux	No	Yes	No	Yes	
Mobility	No	No	Yes	Yes	
Autonomous	No	Yes	No	No	
Field effort	Important	Moderate	Low	Low	
Data processing effort	Low	Moderate	High	Moderate	
Cost range (US\$)	Low-cost	$I_{ow-cost}(un)$	50000 ⁽¹⁾	$10000-50000^{(2)}$	

Table S2: Comparison of four methods with a potential to be used in lake seepage.

_

Cost range (US\$)Low-costLow-cost (un.)50000⁽¹⁾10000-50000⁽²⁾¹Cost excluding video camera and mounting hardware; ²Cost of the detector (the cost of the chamber
assembly was about 300 US\$ in material). un.: undisclosed.50000⁽¹⁾10000-50000⁽²⁾